

# “Pas de deux” of high-temperature alloy and 3D reactor technology for steam cracking of coils: impact on product yields and coke formation

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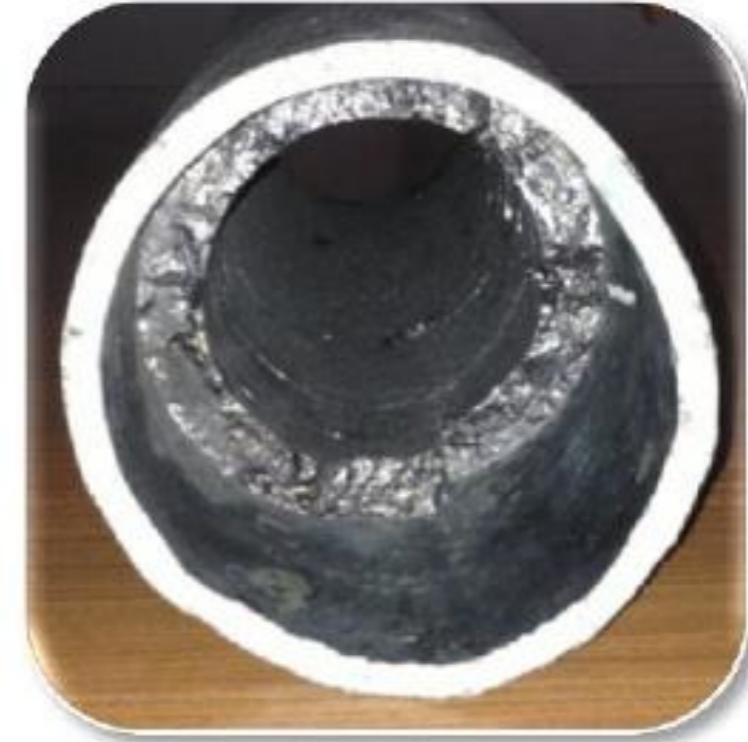
# Outline

- Introduction
- High-temperature alloys and 3D reactor technology
  - Yields
  - Tube metal temperatures
  - Coke formation
- Conclusions

# Coke formation

Deposition of a carbon layer on the reactor surface

-  Thermal efficiency
-  Product selectivity
-  Decoking procedures



[Muñoz, 2013]

Estimated annual cost to industry: \$ 2 billion

Optimization by

- Feed additives
- Metallurgy & surface technology
- 3D reactor technology

L. Benum, "Achieving Longer Furnace Runs at NOVA Chemicals," in AIChE Spring National Meeting, 14th Annual Ethylene Producers' Conference, New Orleans, Louisiana, 2002.

# Outline

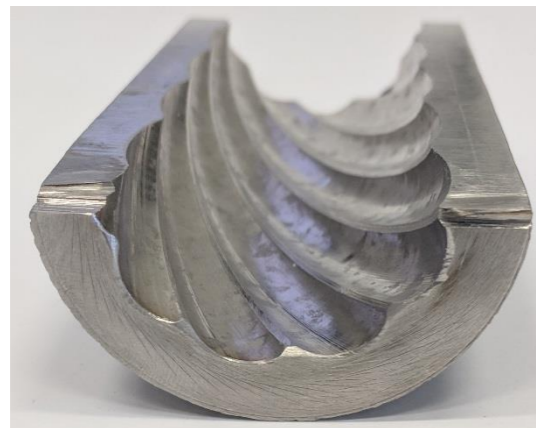
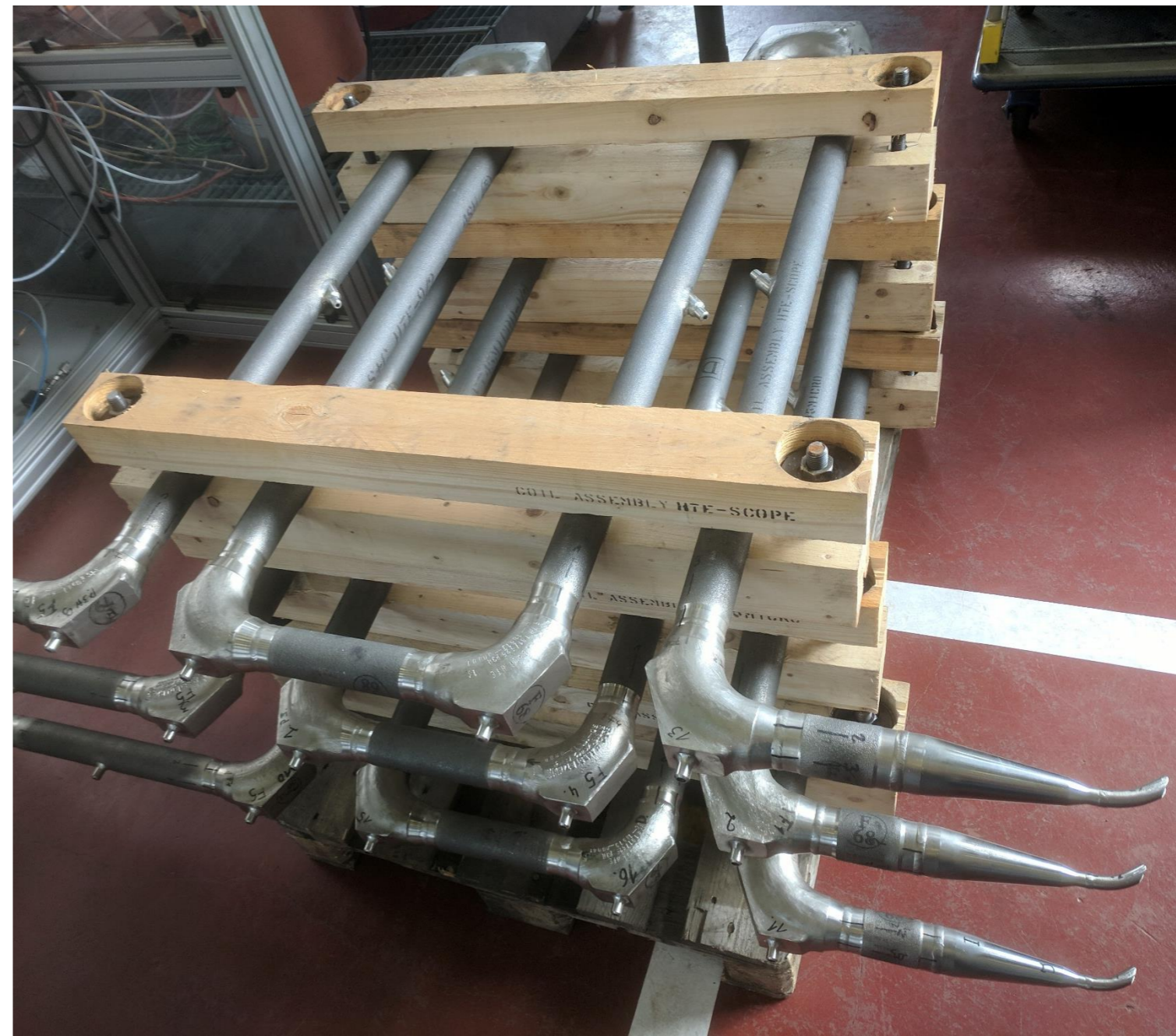
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# Reactors

Centralloy® ET 45 Micro

Centralloy® HT E

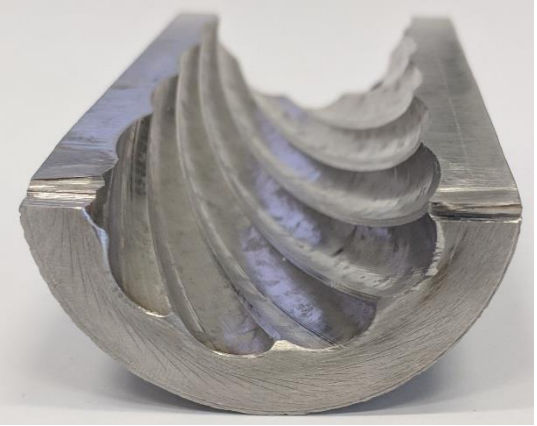
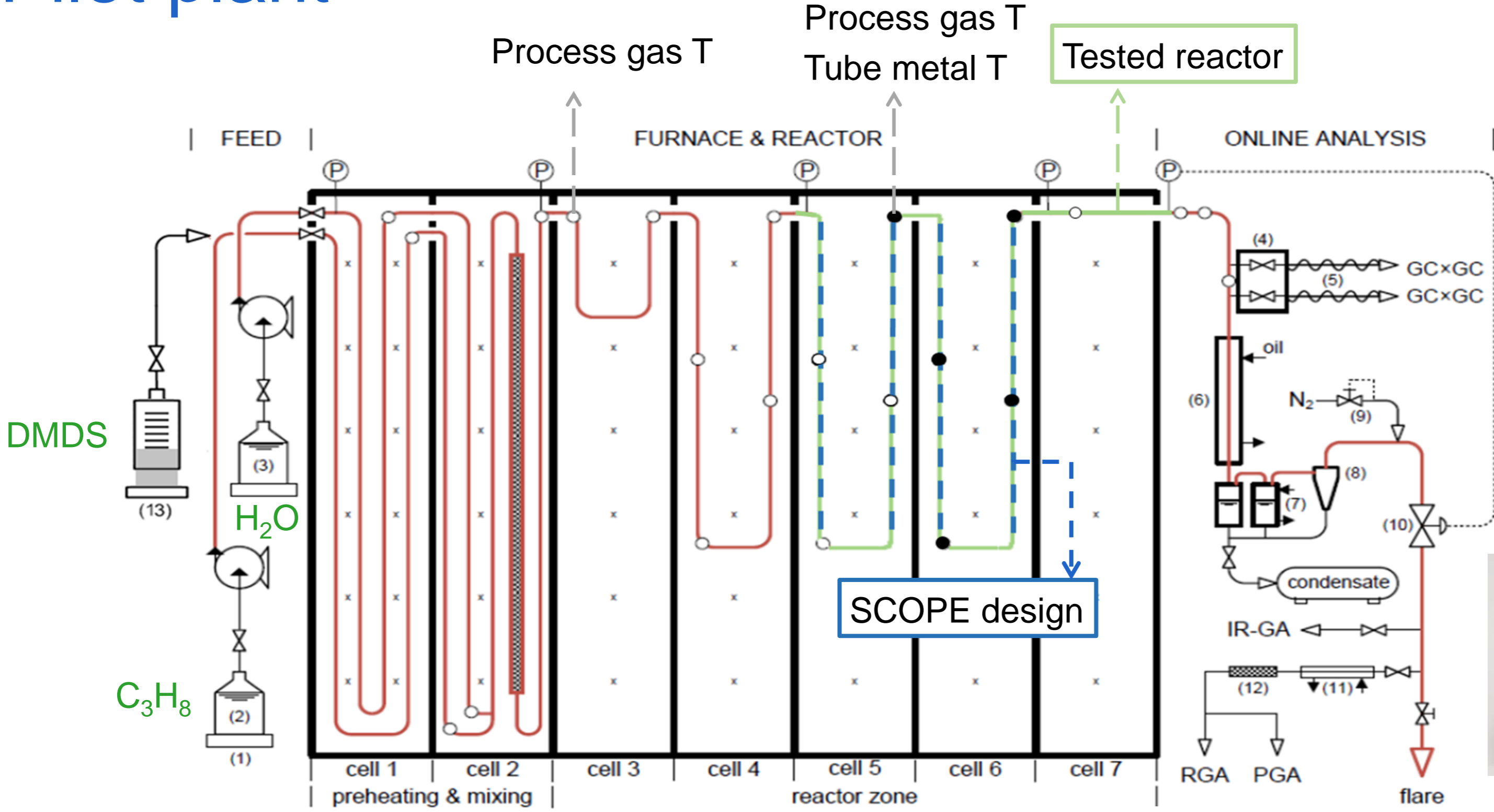
Centralloy® HT E + SCOPE®



Alloy	Composition [wt %]								
	C	Si	Mn	Cr	Fe	Ni	Al	Nb	Additions
ET 45 Micro	0.45	1.6	1.0	35	bal.	45	-	1.0	MAE, RE
HT E	0.45	-	-	30	bal.	45	4.0	0.5	MAE, RE

RE: reactive elements; MAE: micro-alloying elements

# Pilot plant



# Experimental program

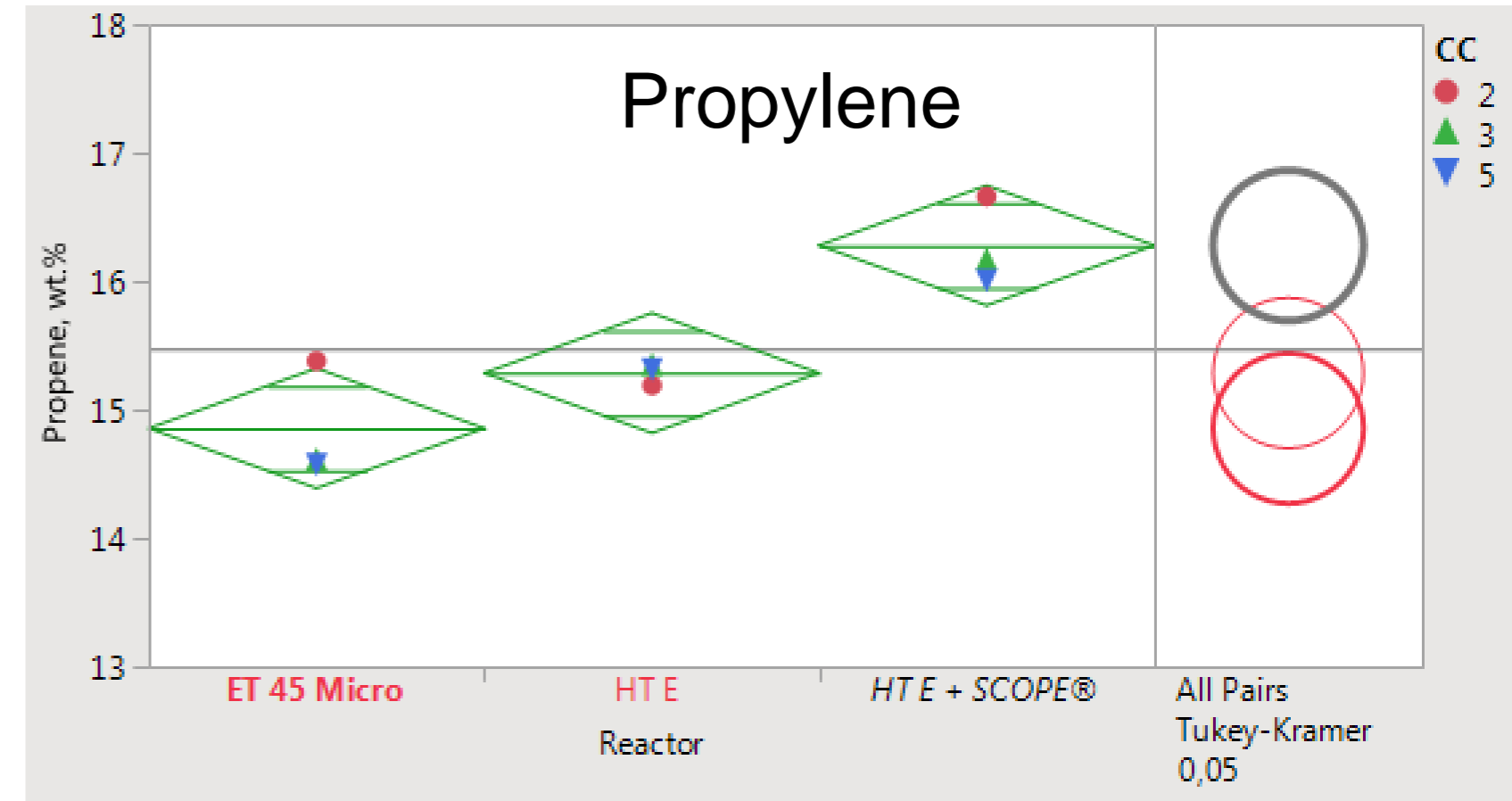
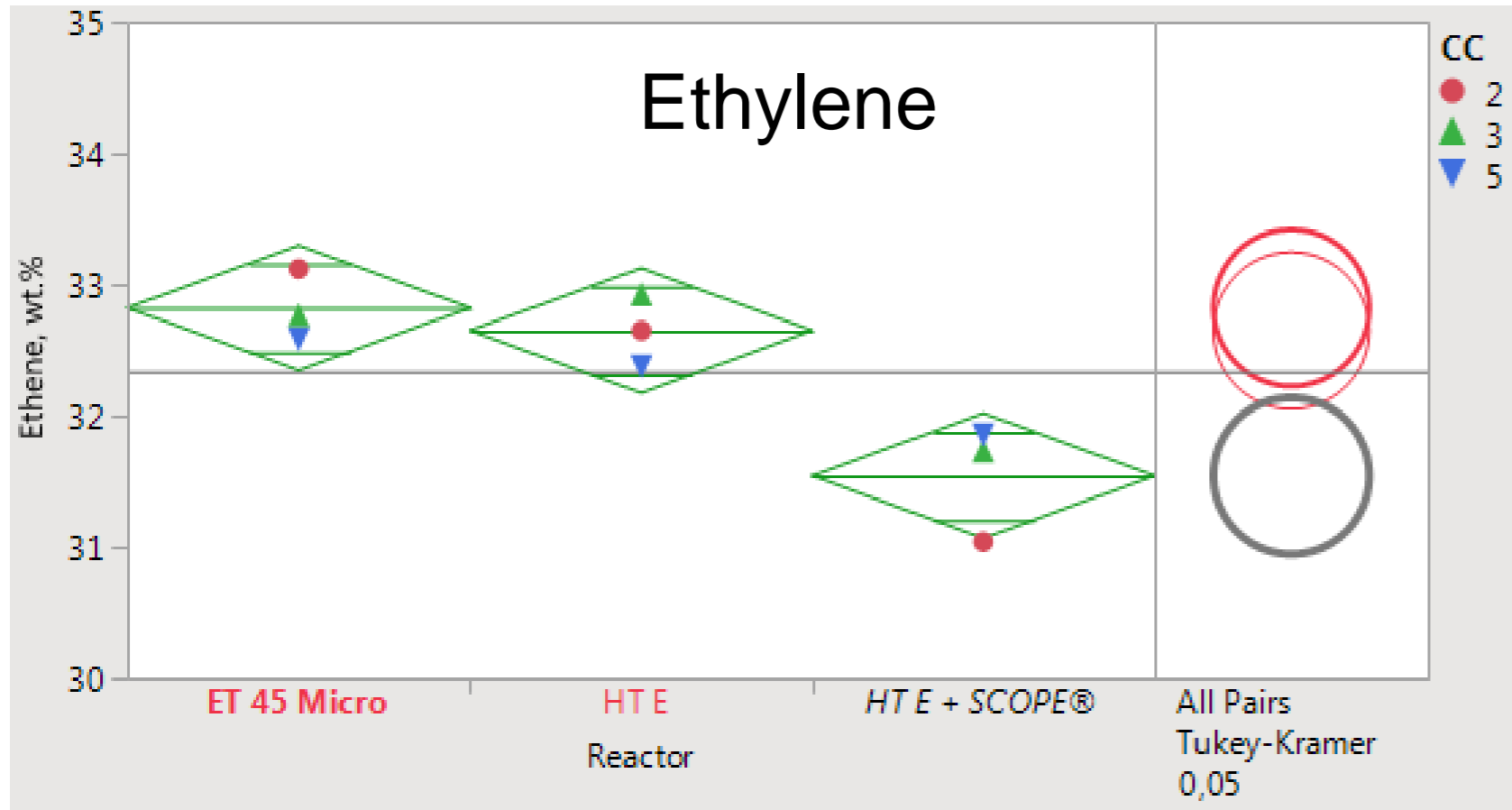
- Steam treatment for 10 hours
- 1CC: COT = base; 6 hours
- 2CC: COT = base; 2 hours
- 3CC: COT = base; 6 hours
- 4CC: COT = base + 110 °C/ + 160 °C\*; 1.67 hours
- 5CC: COT = base; 12 hours

\*SCOPE<sup>®</sup>

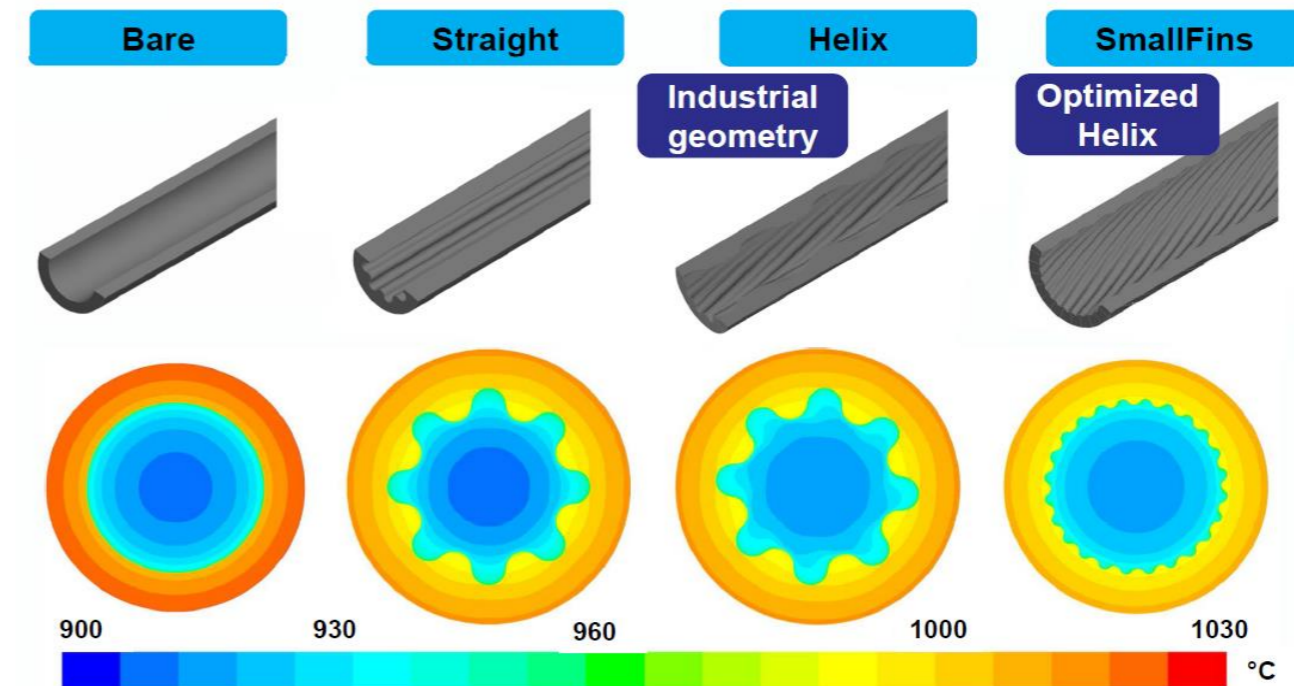
- ✓ Decoking was performed after every Cracking Cycle (CC)
- ✓ Prior to each CC a pre-sulfiding step was performed

# Product yields

2 (CC2), 6 (CC3) and 12 h (CC5) cracking cycles

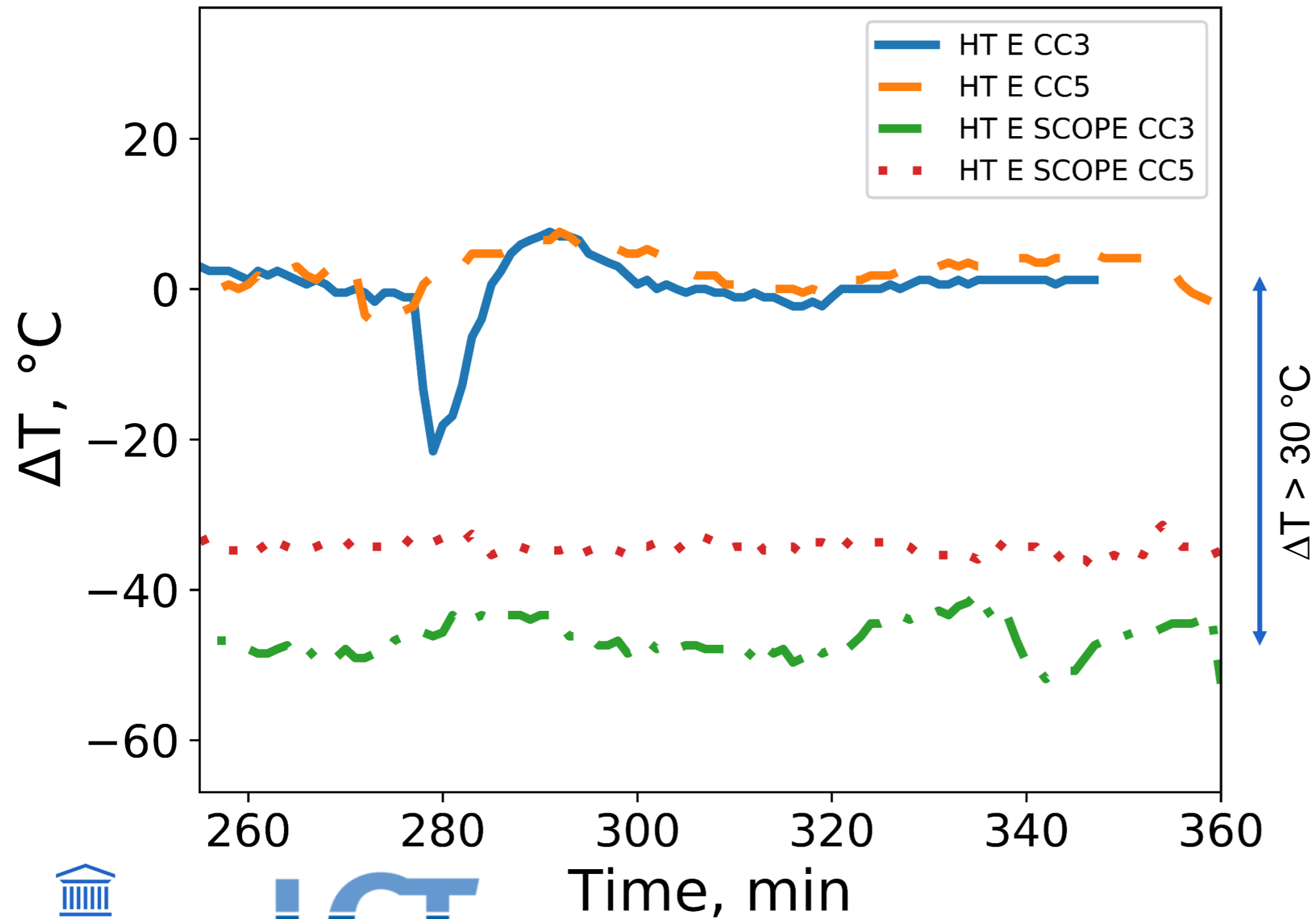


Reduced over-cracking near wall





# Tube metal temperatures



Pyrometer



Weld-on TC's

Gas consumption



**Result**

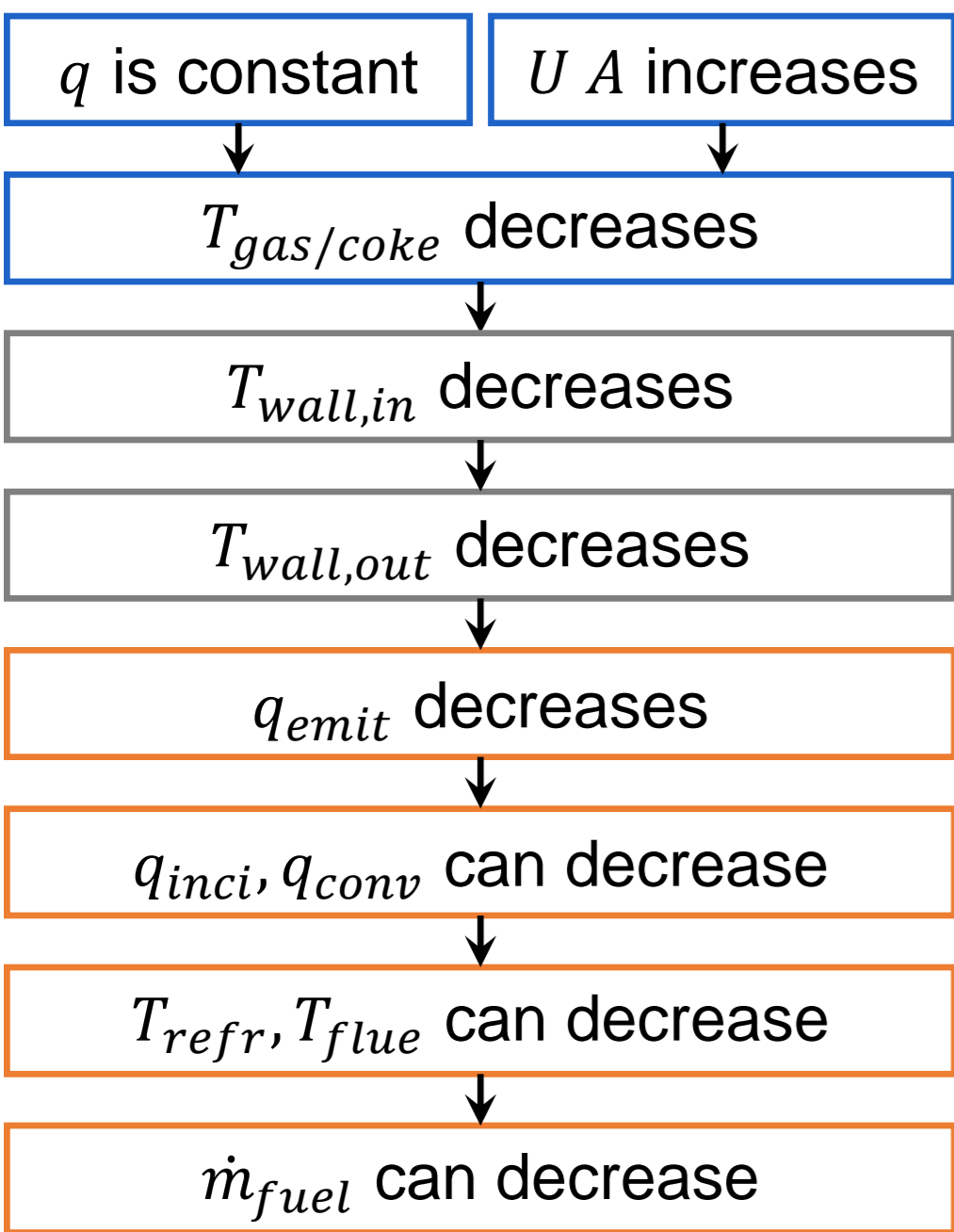
~10 % lower  
Fuel gas consumption

Manual T



# Tube metal temperatures

30°C lower tube metal temperature reduces fuel consumption by ~10%



Convection on inner wall

$$q = U A (T_{gas/coke} - T_{bulk})$$

Conduction through coke

$$q = k_c A (T_{wall,in} - T_{gas/coke}) / d_c$$

Conduction through metal

$$q = k_m A (T_{wall,out} - T_{wall,in}) / d_m$$

Heat balance on outer wall

$$q = [q_{inci} - q_{re} + q_{conv}] - q_{emit}$$

$$\varepsilon_w q_{inci} + q_{conv}$$

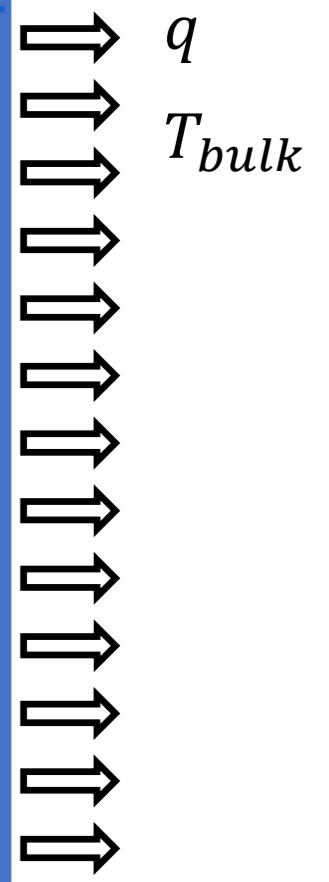
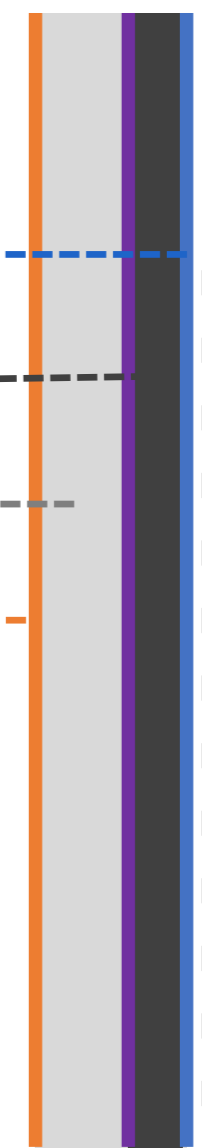
$$\varepsilon_w \sigma T_{wall,out}^4$$

$$\sim T_{refr}, T_{flue}$$

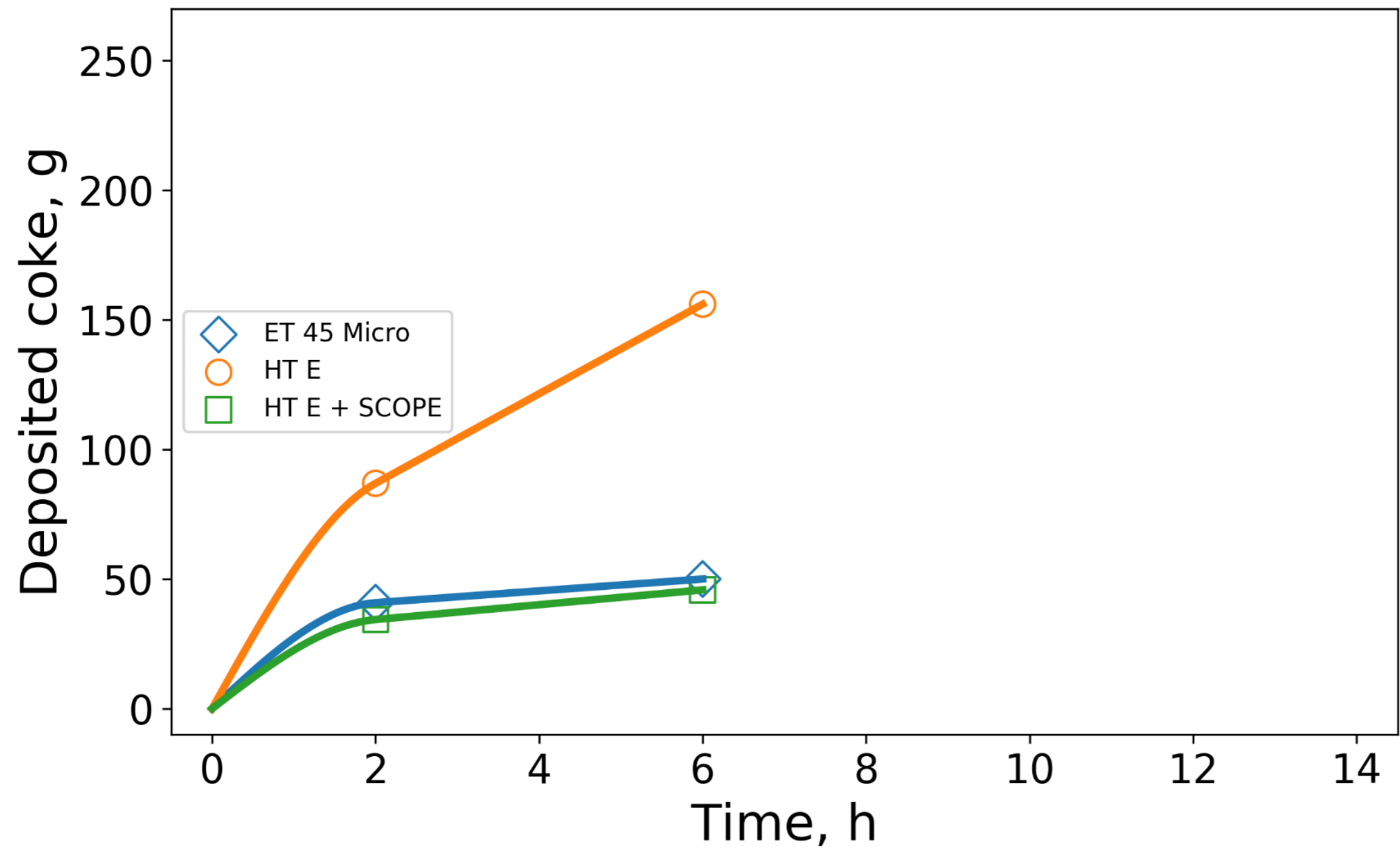
$$\sim \dot{m}_{fuel}$$

Flue gas side

Process gas side



# Coke deposition



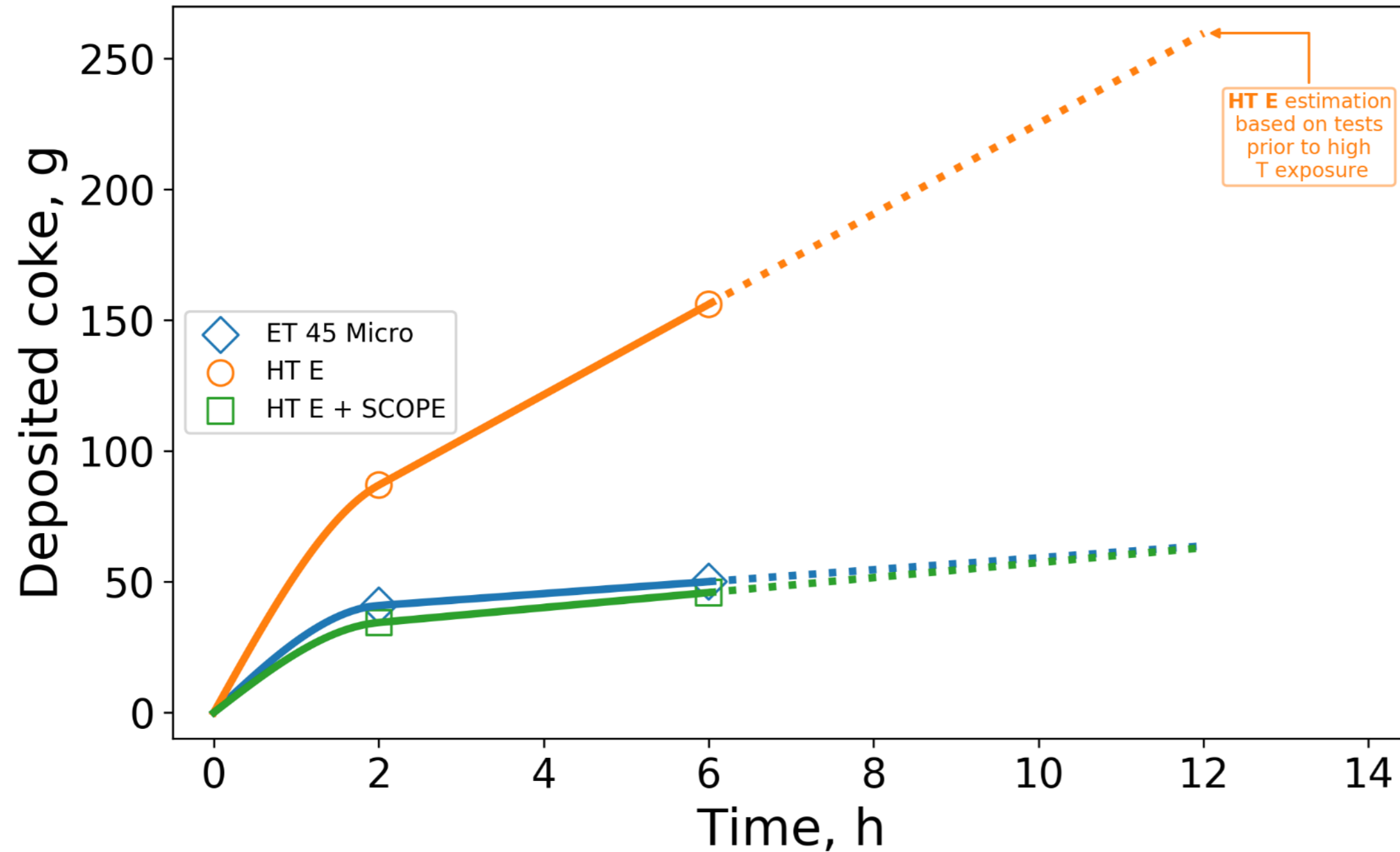
Coke after 2 (CC2) and 6h (CC3)

ET 45 Micro and HT E + SCOPE  
comparable

HT E significantly worse

Line: estimated coking curve

# Coke deposition



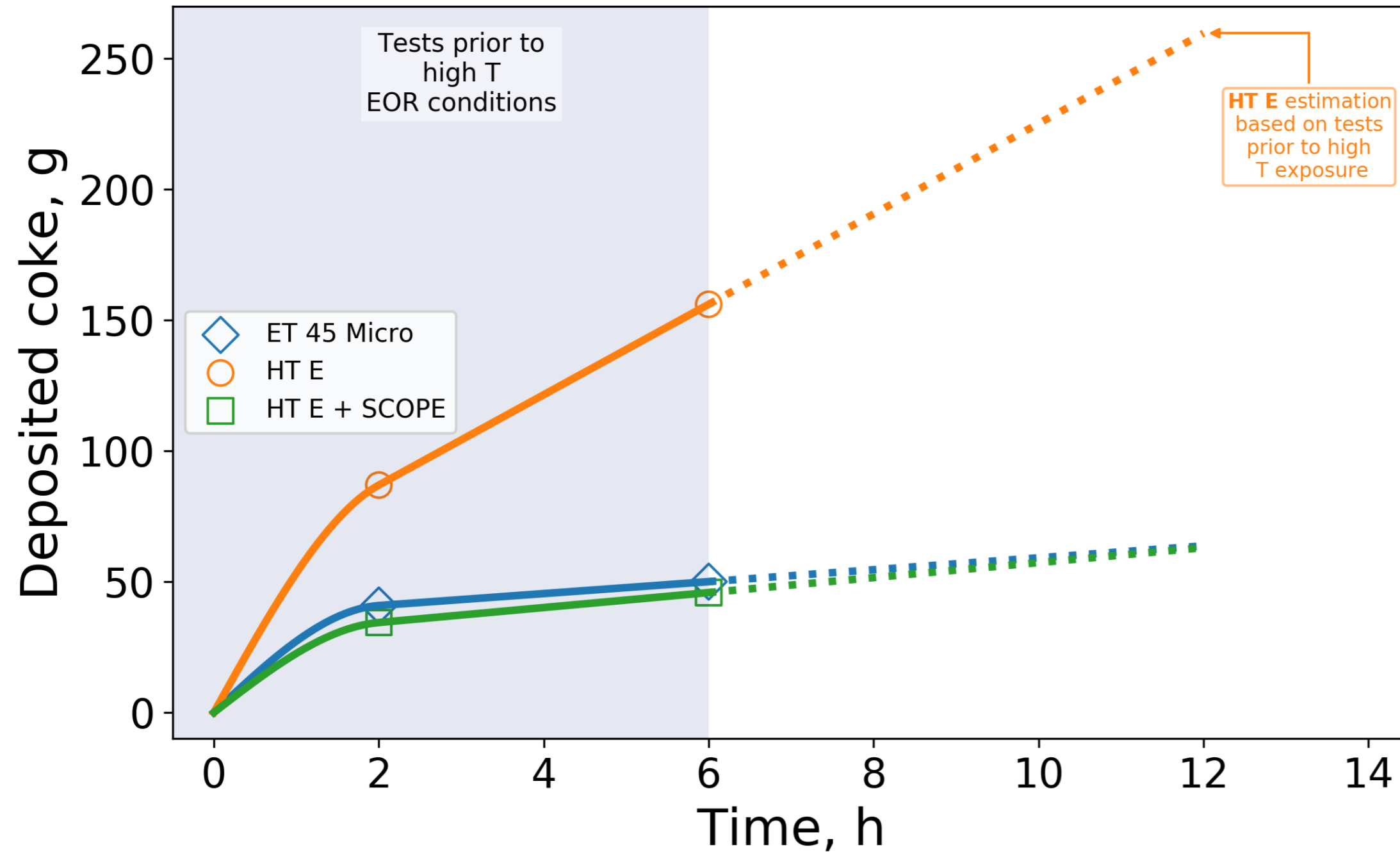
Extrapolation for 12 h coke

Assumptions:

2 h (CC2) = Catalytic

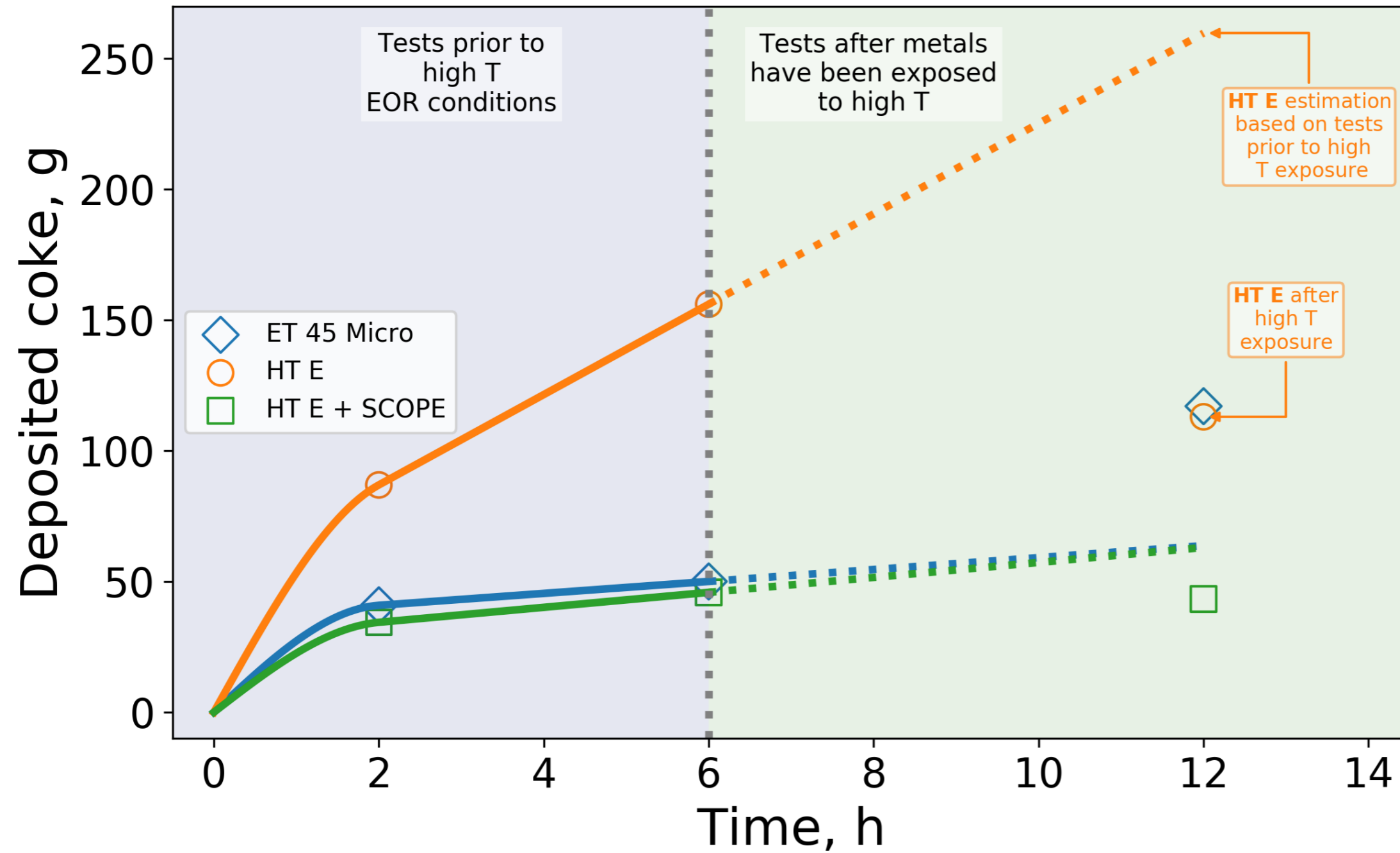
6 h (CC3) = asymptotic

# Coke deposition



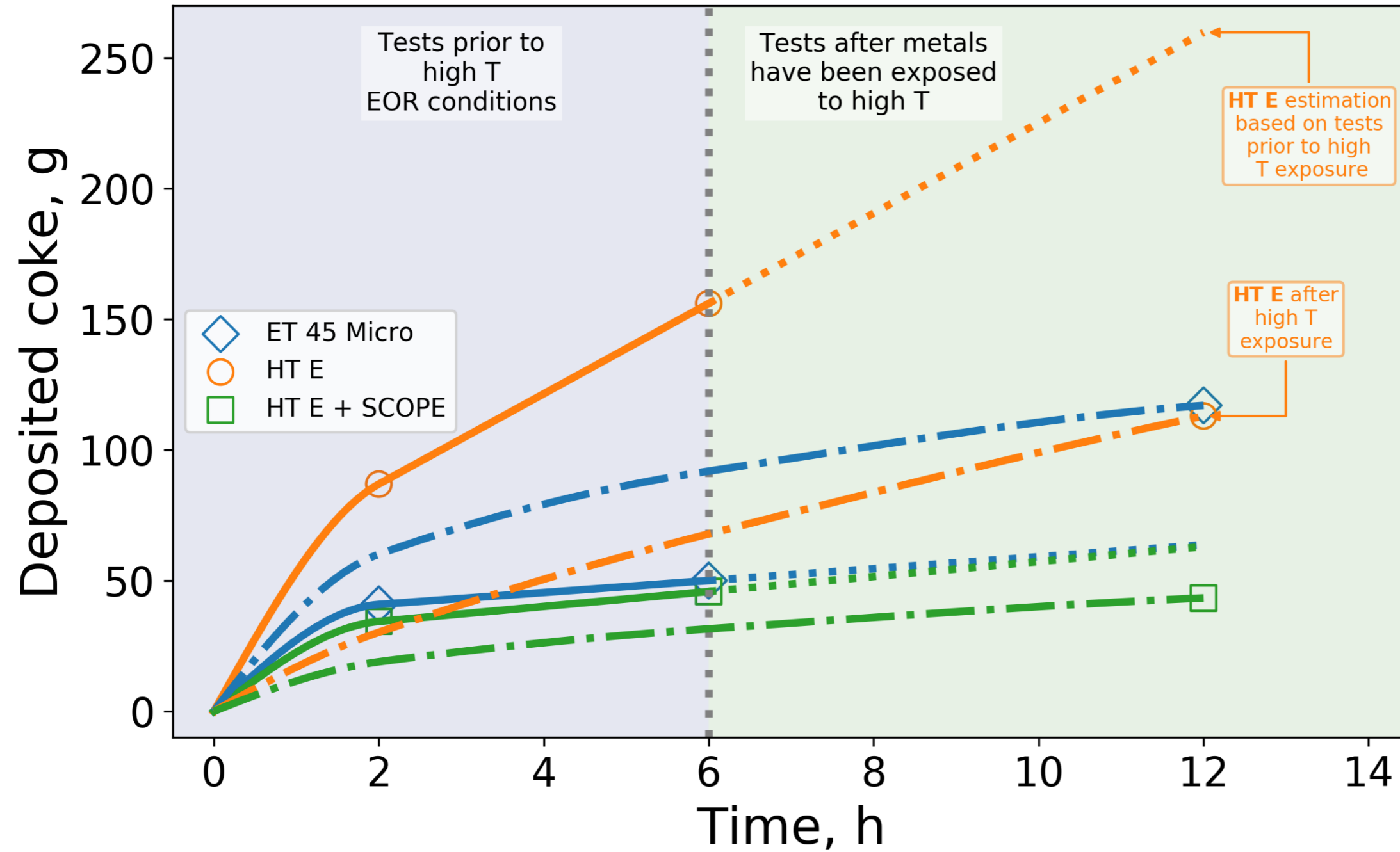
Extrapolation based on tests prior to high T (EOR) exposure

# Coke deposition



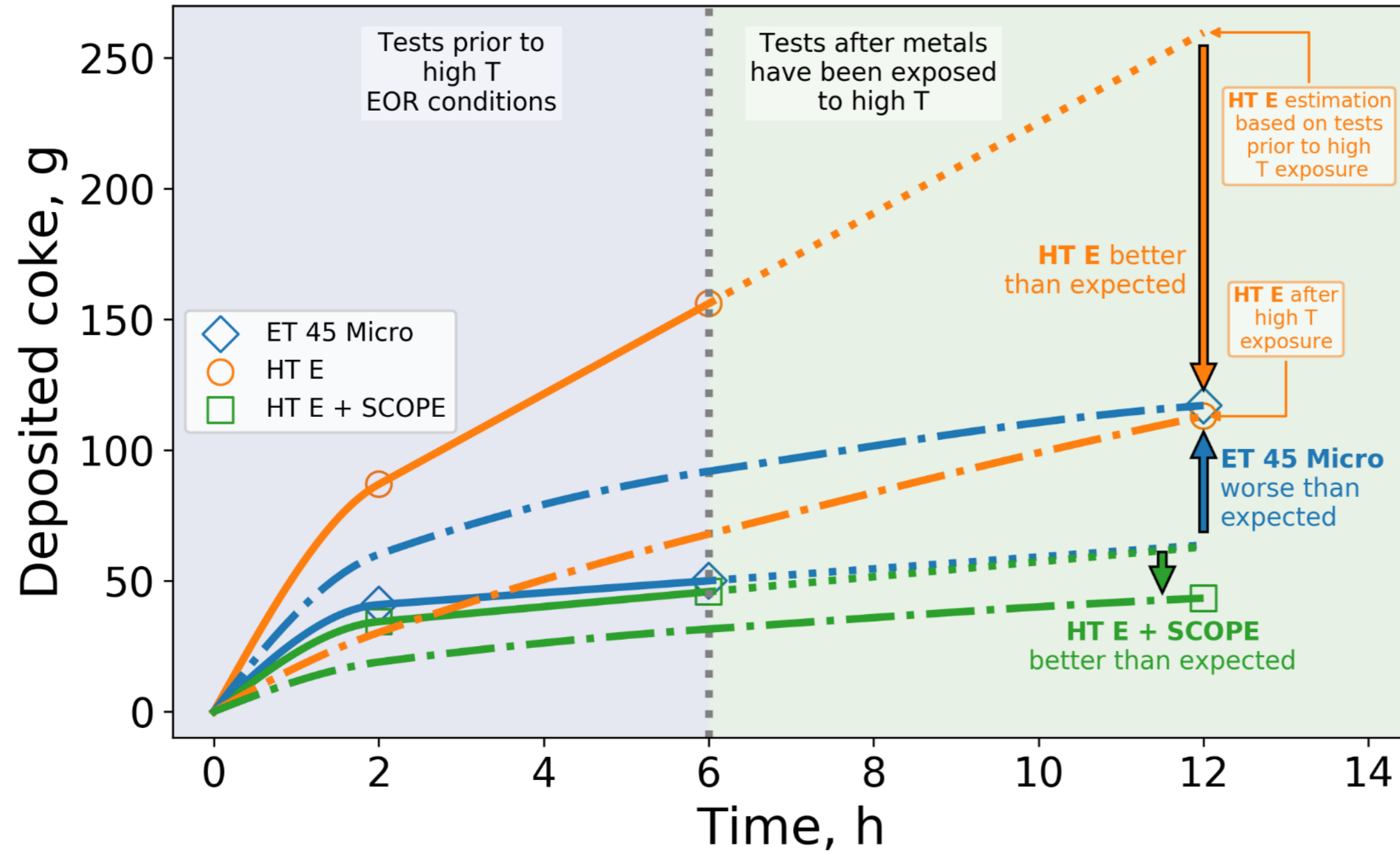
Coke after high T exposure

# Coke deposition



Estimation coking curve

# Coke deposition



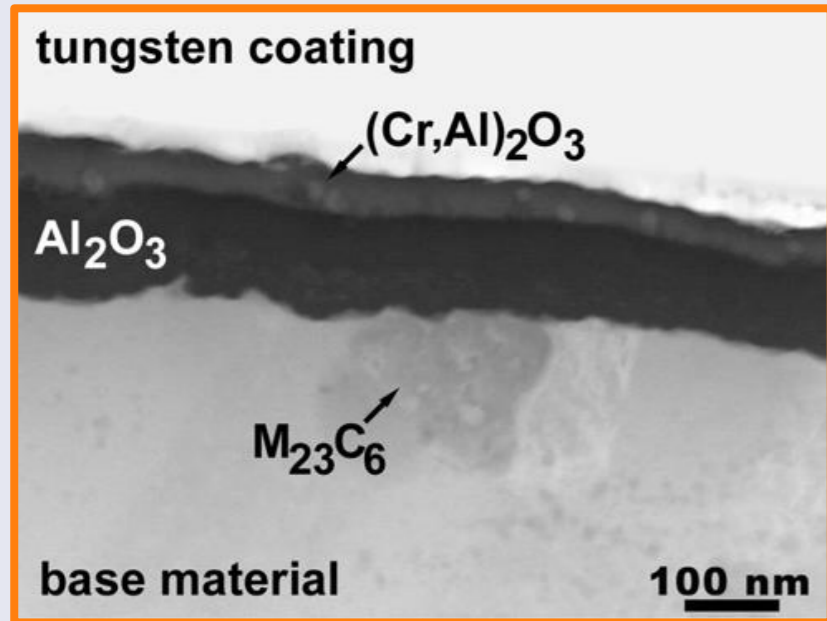
HT E better than expected

ET 45 Micro worse than expected

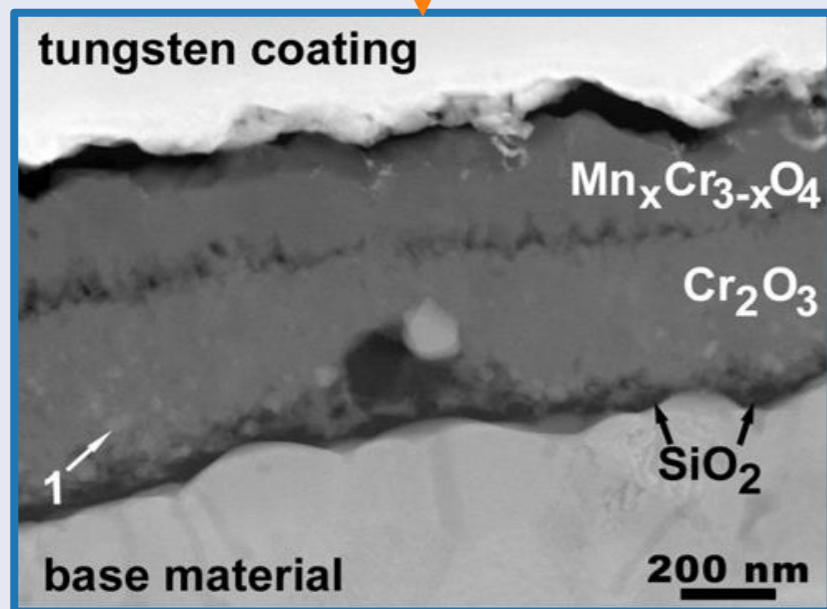
SCOPE design →  
Lower temperatures  
Lower influence high T excursion



# Coke deposition

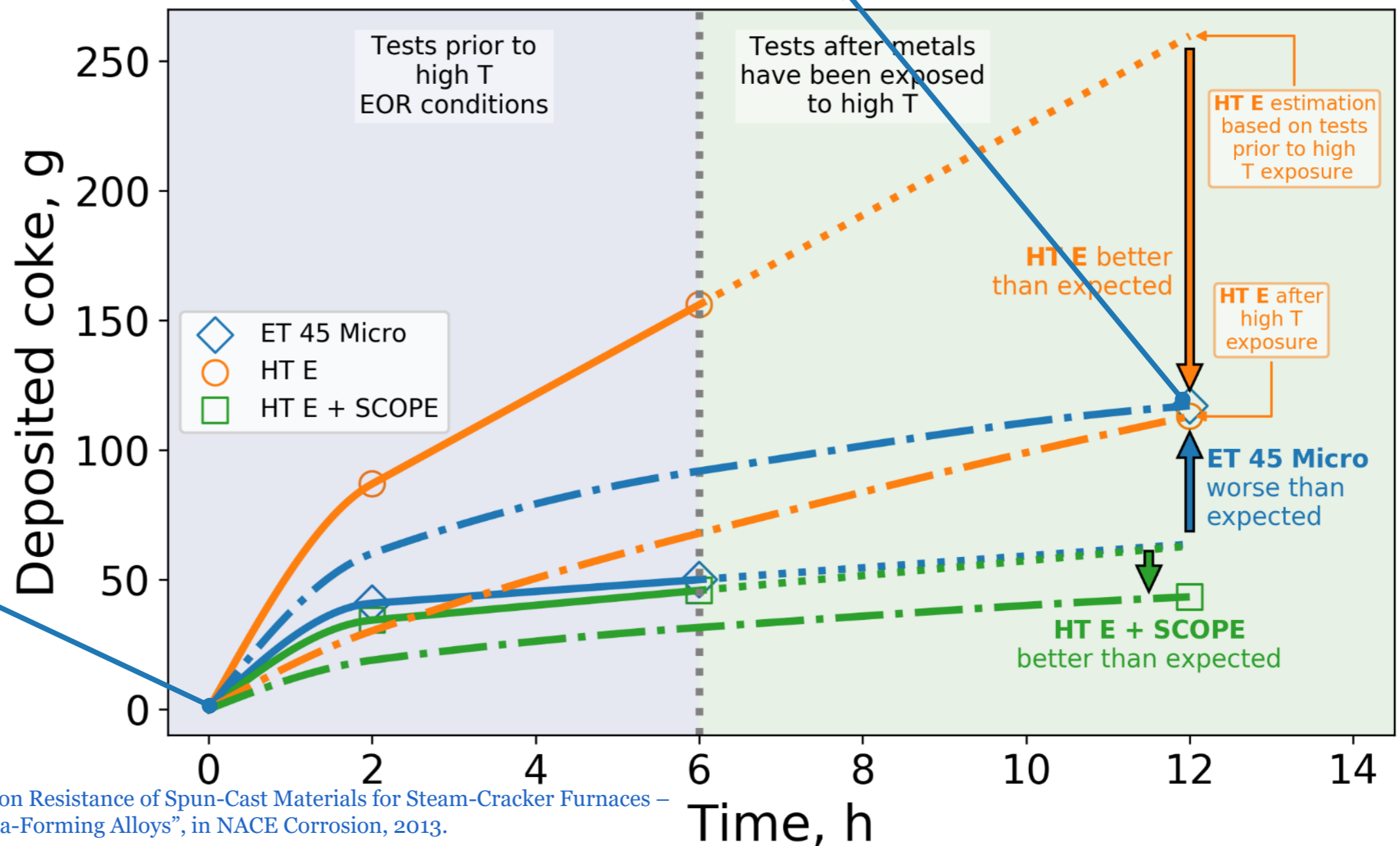
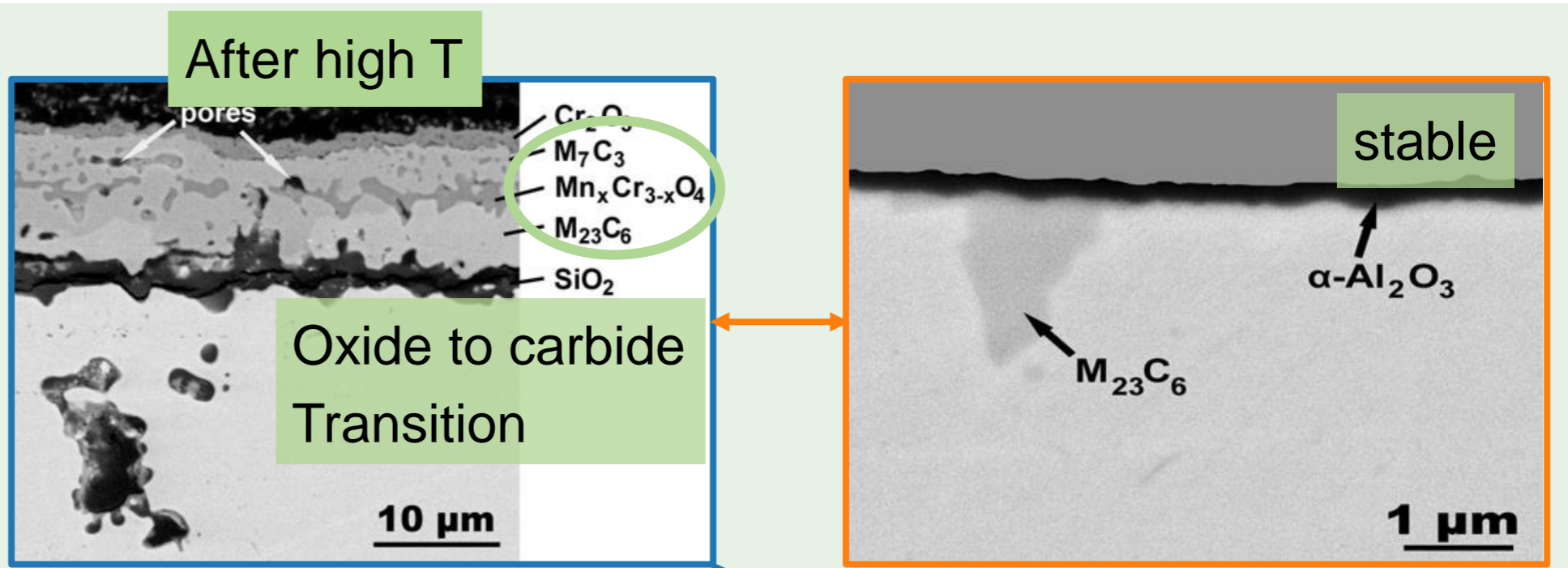


HT E



ET 45 Micro

After pre-Ox  
Before high T



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# Conclusion

- After high Temperature (EOR) exposure **HT E** performs **better**, while the performance of **ET 45 Micro drops**
- **ET 45 Micro** → Oxide to carbide transition
- **HT E** → Formation stable  $\alpha\text{-Al}_2\text{O}_3$  scale
- Combining the advanced coil material (**HT E**) and novel 3D reactor design (**SCOPE<sup>®</sup>**) leads to
  - Increased run lengths
  - Improved product selectivities
  - Longer lifetime of the reactor coils
  - Higher energy efficiency of the furnace

# Acknowledgments

The work leading to this intervention has received funding from the European Union H2020 (H2020-SPIRE-04-2016) under grant agreement n°723706 and from the COST Action CM1404 “Chemistry of smart energy carriers and technologies”.



Thank you for your attention!

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# GLOSSARY

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