

FACULTY OF ENGINEERING AND
ARCHITECTURE

Quantitative first principles based kinetic modeling for the synthesis of well-defined macromolecular architectures

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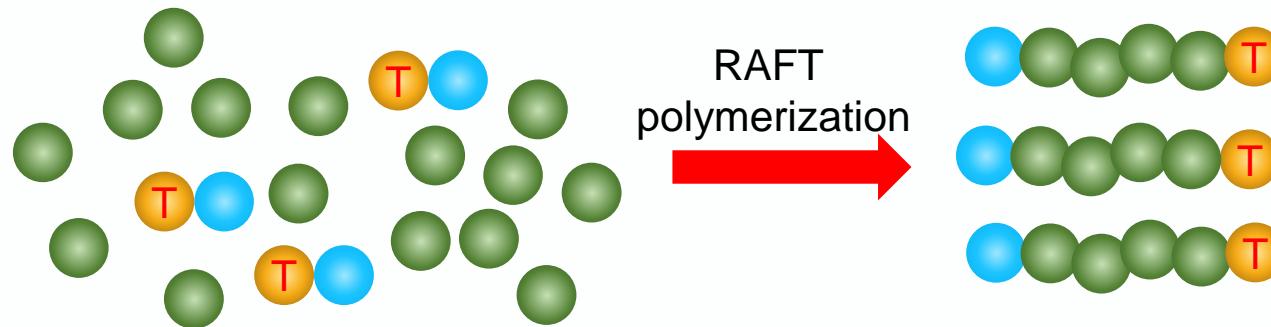
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<http://www.lct.UGent.be>

Contents: 2 case studies related to Reversible Addition-Fragmentation chain Transfer (RAFT) polymerization

1. RAFT polymerization of styrene (●) using a trithiocarbonate (○T○)

 - Calculation of **addition-fragmentation** rate coefficients
 - Application in a **microkinetic model**

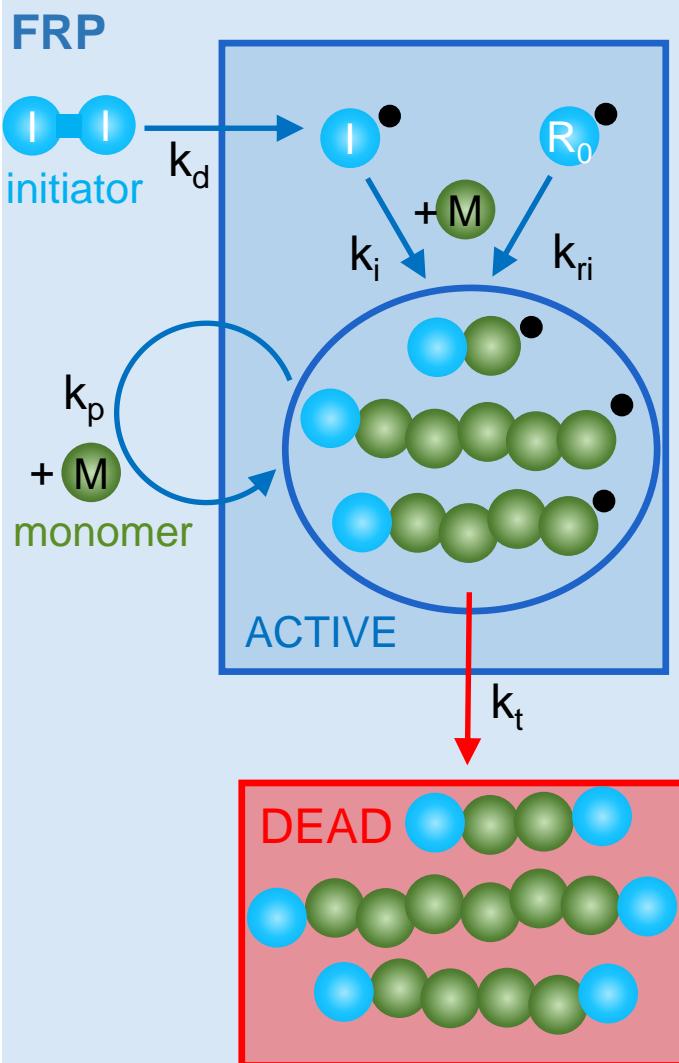


2. The **aminolysis of RAFT-macromolecules**

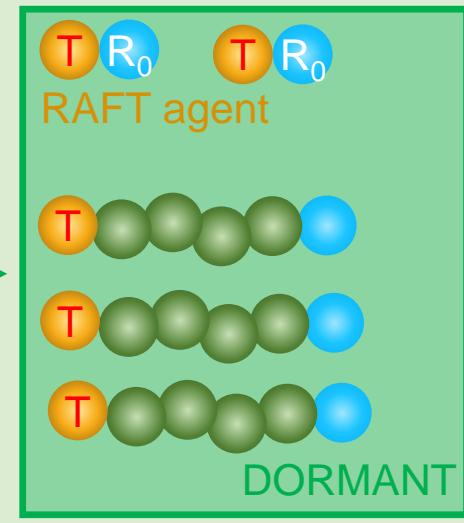
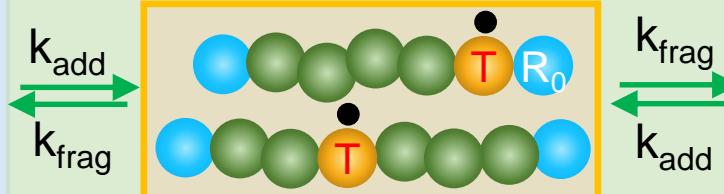
- Determination of the reaction mechanism
- calculation of **rate coefficients** for a variety of RAFT-agents



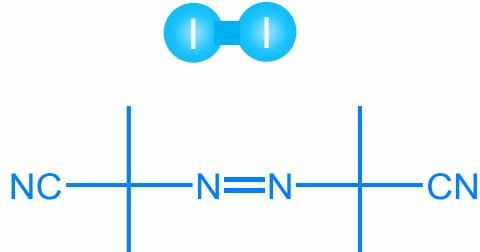
How do RAFT agents help us to obtain control over the chain length in radical polymerization



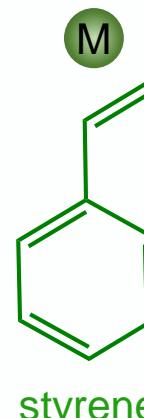
RAFT exchange



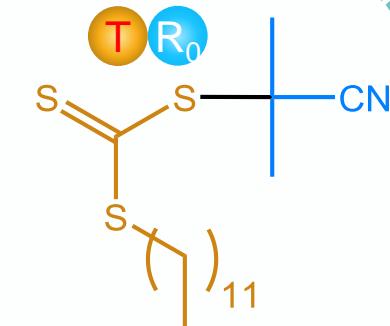
used in this work



azobisisobutyro
nitrile (AIBN)

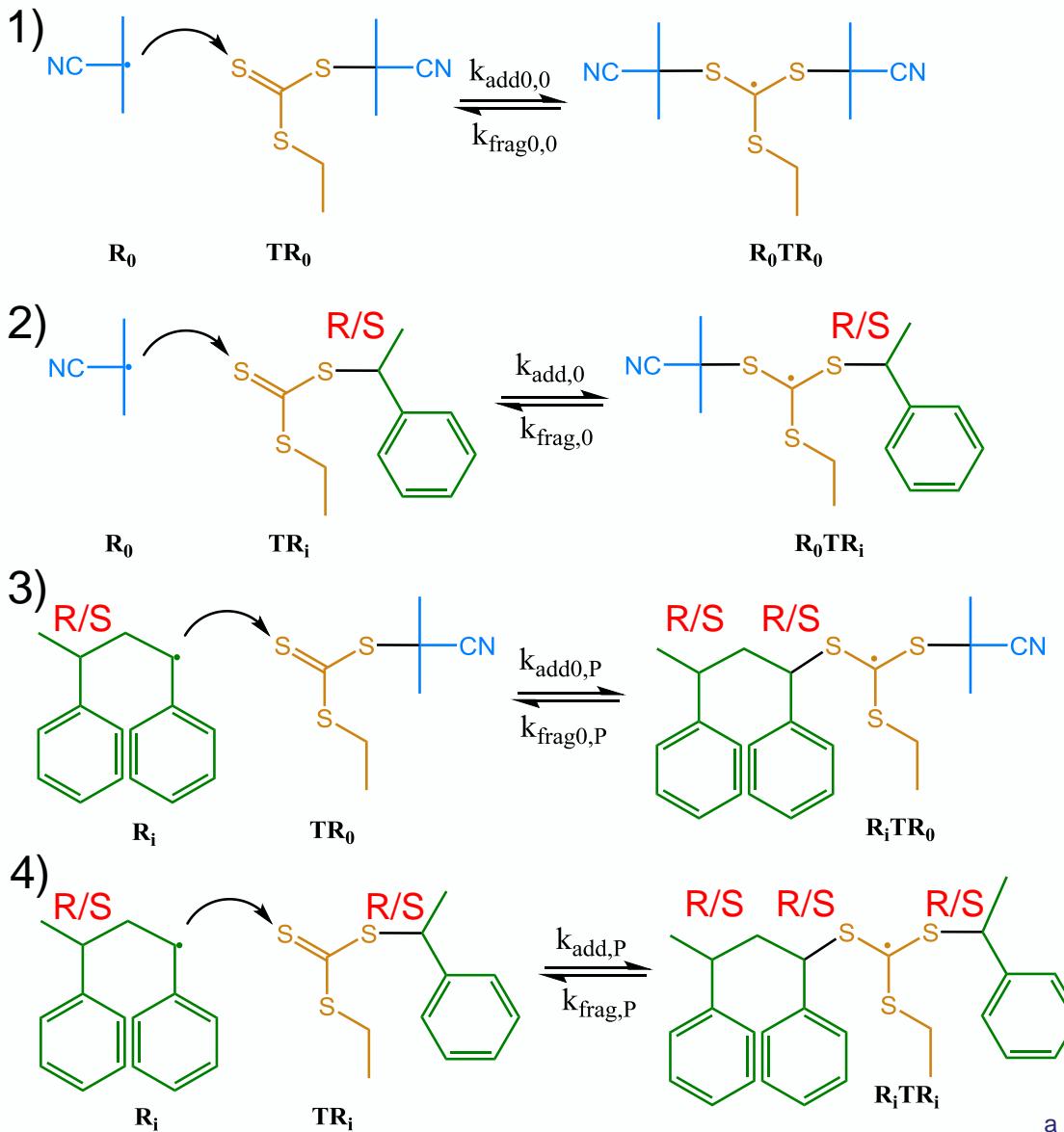


styrene



2-cyano-2-propyl-
dodecyl trithio-
carbonate (CPDT)

Ab initio calculation of addition-fragmentation reactions using a dimer model: 4 model reactions



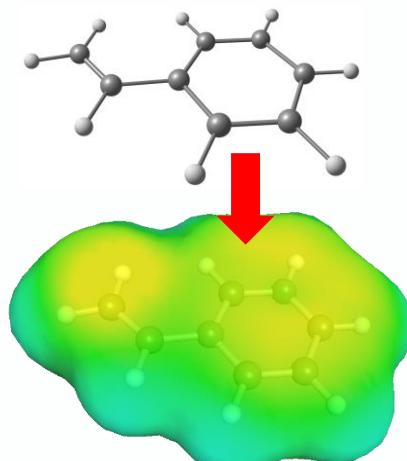
Model assumptions

- dimer radical to model macroradical
- ethyl group to model dodecyl group

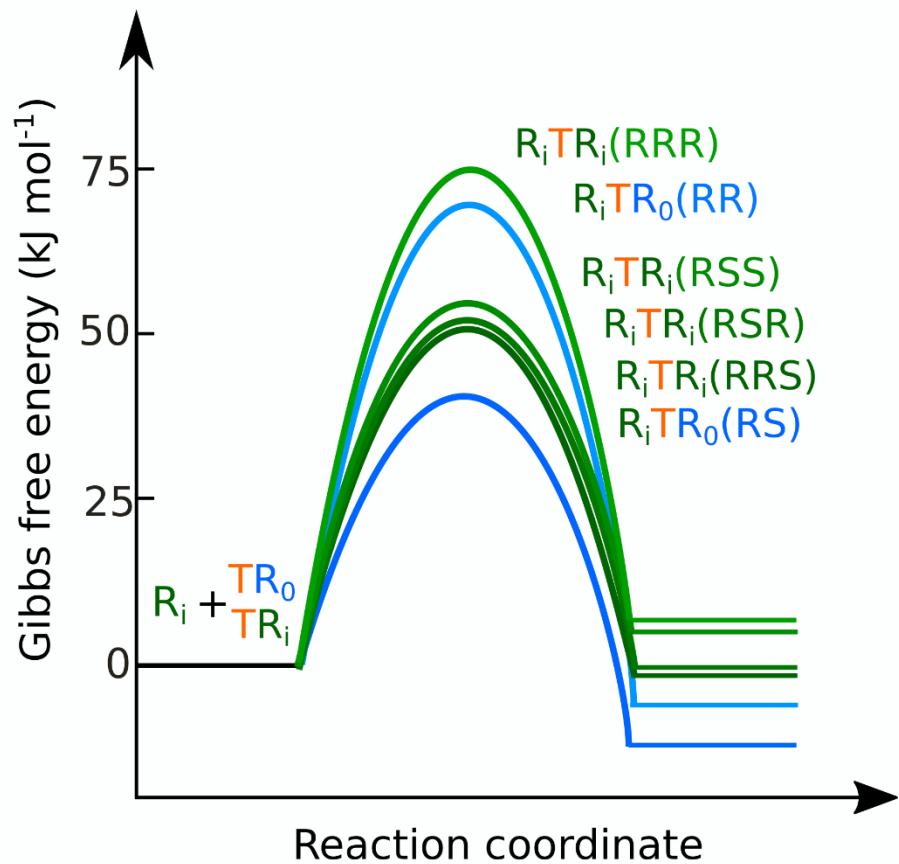
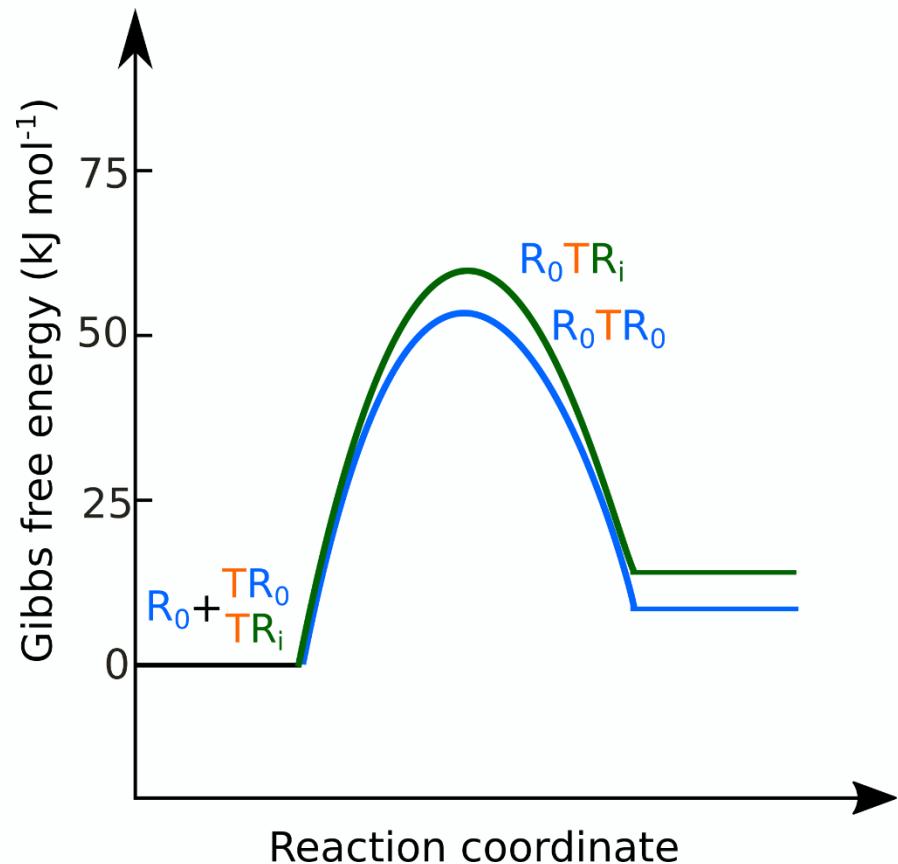
Ab initio calculation

- scan conformers: B3LYP/6-31G(d)
- geometry optimization and frequencies: B3LYP/6-31G(d)
- ‘single point’ electronic energy: M06-2X/6-311+G(d,p)

Solvation via COSMO-RS



Gibbs free energy diagrams of the addition-fragmentation reactions



- Rate coefficients are obtained via classical transition state theory:

$$K = e^{\frac{-\Delta_r G^\circ}{RT}} \quad k_+ = \frac{k_B T}{h} e^{\frac{-\Delta^\ddagger G^\circ}{RT}} \quad k_- = k_+/K$$

- Stereoisomers are taken into account according to the following formulas:

$$k_{add} = \frac{1}{n_0} \sum_i k_{add,i} \quad k_{frag} = \frac{\sum_i k_{frag,i} K_i}{\sum_i K_i}$$

Deterministic kinetic model based on methods of moments^a

FRP
RAFT

Reaction	Equation	E_a kJ mol ⁻¹	A L mol ⁻¹ s ⁻¹
Dissociation*	$I_2 \rightarrow 2R_0$	129.0	1.6×10^{15} ^d
(Re)Initiation	$R_0 + M \rightarrow R_1$	26.0	4.9×10^7 ^e
Propagation	$R_i + M \rightarrow R_{i+1}$	32.5	4.2×10^7 ^f
Combination**	$R_i + R_j \rightarrow R_{i+j}$	0.0	5.0×10^8 ^g
Addition	$R_0 + TR_0 \rightarrow R_0 TR_0$	13.9	7.4×10^6
Addition	$R_0 + TR_i \rightarrow R_0 TR_i$	24.2	1.6×10^7
Addition	$R_i + TR_0 \rightarrow R_i TR_0$	3.0	9.4×10^6
Addition	$R_i + TR_i \rightarrow R_i TR_i$	15.4	1.7×10^7
Fragmentation	$R_0 TR_0 \rightarrow R_0 + TR_0$	44.6	9.4×10^{12}
Fragmentation	$R_0 TR_i \rightarrow R_0 + TR_i$	48.3	1.2×10^{13}
Fragmentation	$R_i TR_0 \rightarrow R_i + TR_0$	51.7	2.6×10^{12}
Fragmentation	$R_i TR_i \rightarrow R_i + TR_i$	53.2	1.2×10^{13}

* Initiator efficiency^b

$$f_{app} = \frac{D_I}{D_I + D_{term}}$$

** Diffusional limitations

Via composite k_t model^c

- for $i < i_{gel}$ and $i < i_{SL}$:

$$k_{t,ii}^{app} = k_{t,11} i^{-\alpha_s}$$

- for $i < i_{gel}$ and $i \geq i_{SL}$:

$$k_{t,ii}^{app} = k_{t,11} i_{SL}^{\alpha_l - \alpha_s} i^{-\alpha_l}$$

- for $i \geq i_{gel}$ and $i < i_{SL}$:

$$k_{t,ii}^{app} = k_{t,11} i_{gel}^{\alpha_{gel} - \alpha_s} i^{-\alpha_{gel}}$$

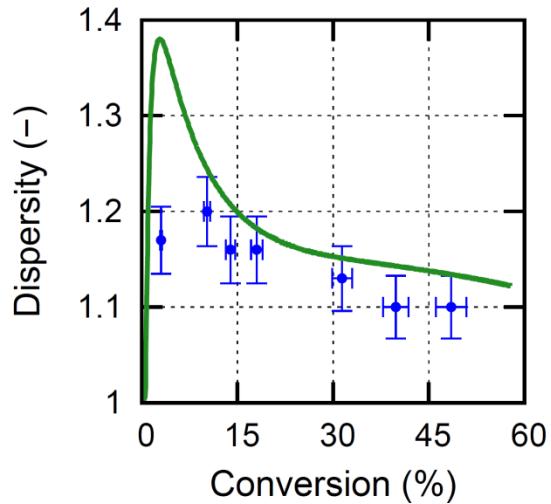
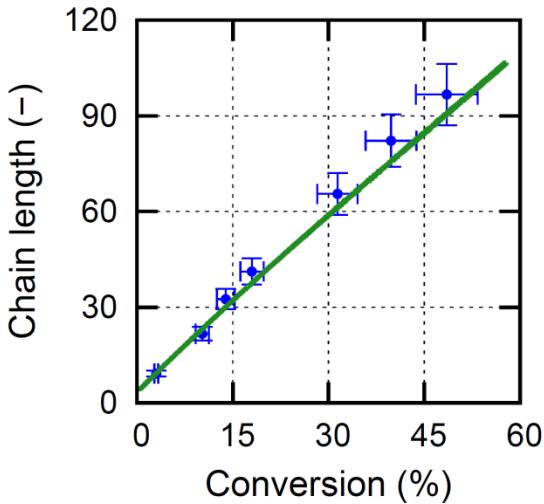
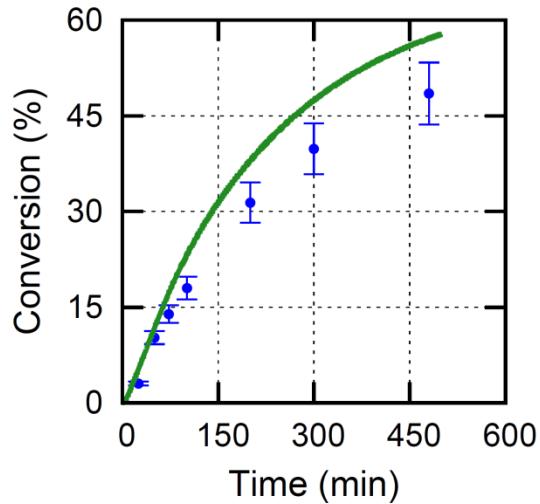
- for $i \geq i_{gel}$ and $i \geq i_{SL}$:

$$k_{t,ii}^{app} = k_{t,11} i_{SL}^{\alpha_l - \alpha_s} i_{gel}^{\alpha_{gel} - \alpha_l} i^{-\alpha_{gel}}$$

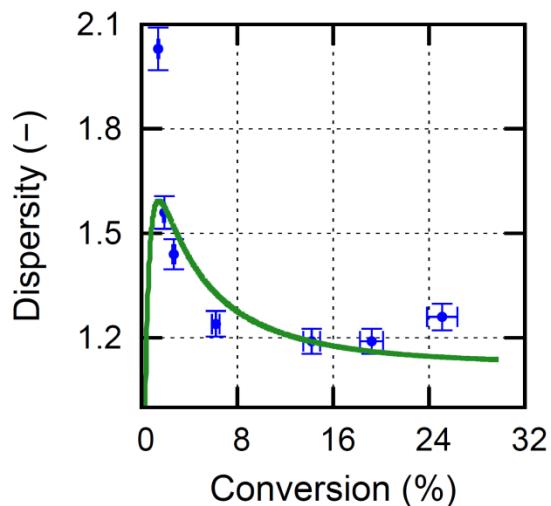
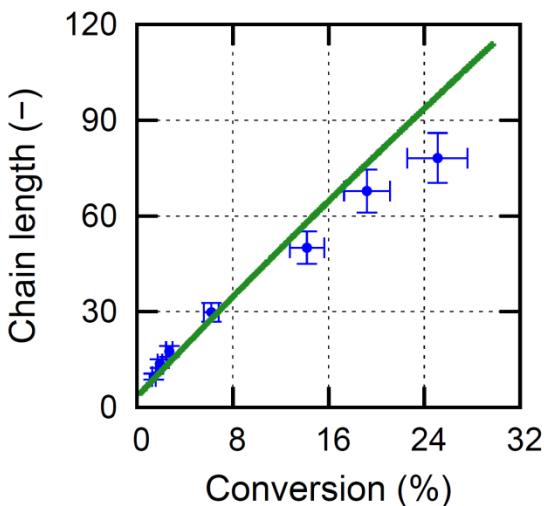
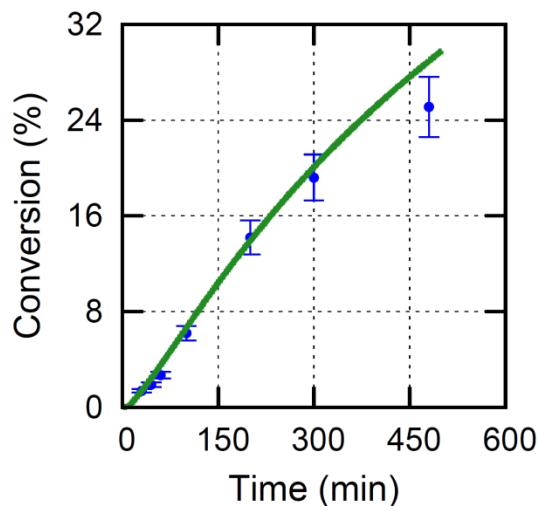
^a De Rybel et al., *Macromol. Theor. Simul.* 2016, *in press*; ^b Buback et al., *Macromol. Chem. Phys.* 1994, 195, 2117; ^c Johnston-Hall and Monteiro, *J. Polym. Sci. Polym. Chem.* 2008, 46, 3155-3173; ^d Van Hook et al., *J. Am. Chem. Soc.* 1958, 80, 779–782; ^e Héberger et al., *Int. J. Chem. Kinet.* 1993, 25, 249–263; ^f M. Buback, *Macromol. Chem. Phys.* 1995, 196, 3267–3280; ^g Johnston-Hall et al., *Macromolecules*, 2008, 41, 727–736

Simulation and experimental validation

$T = 80 \text{ }^{\circ}\text{C}$, TCL = 200, CTA:AIBN = 5:1



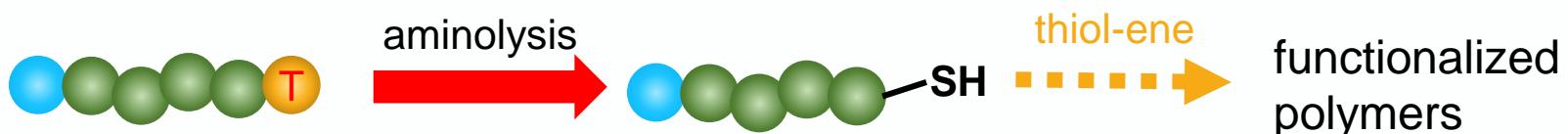
$T = 70 \text{ }^{\circ}\text{C}$, TCL = 400, CTA:AIBN = 5:1



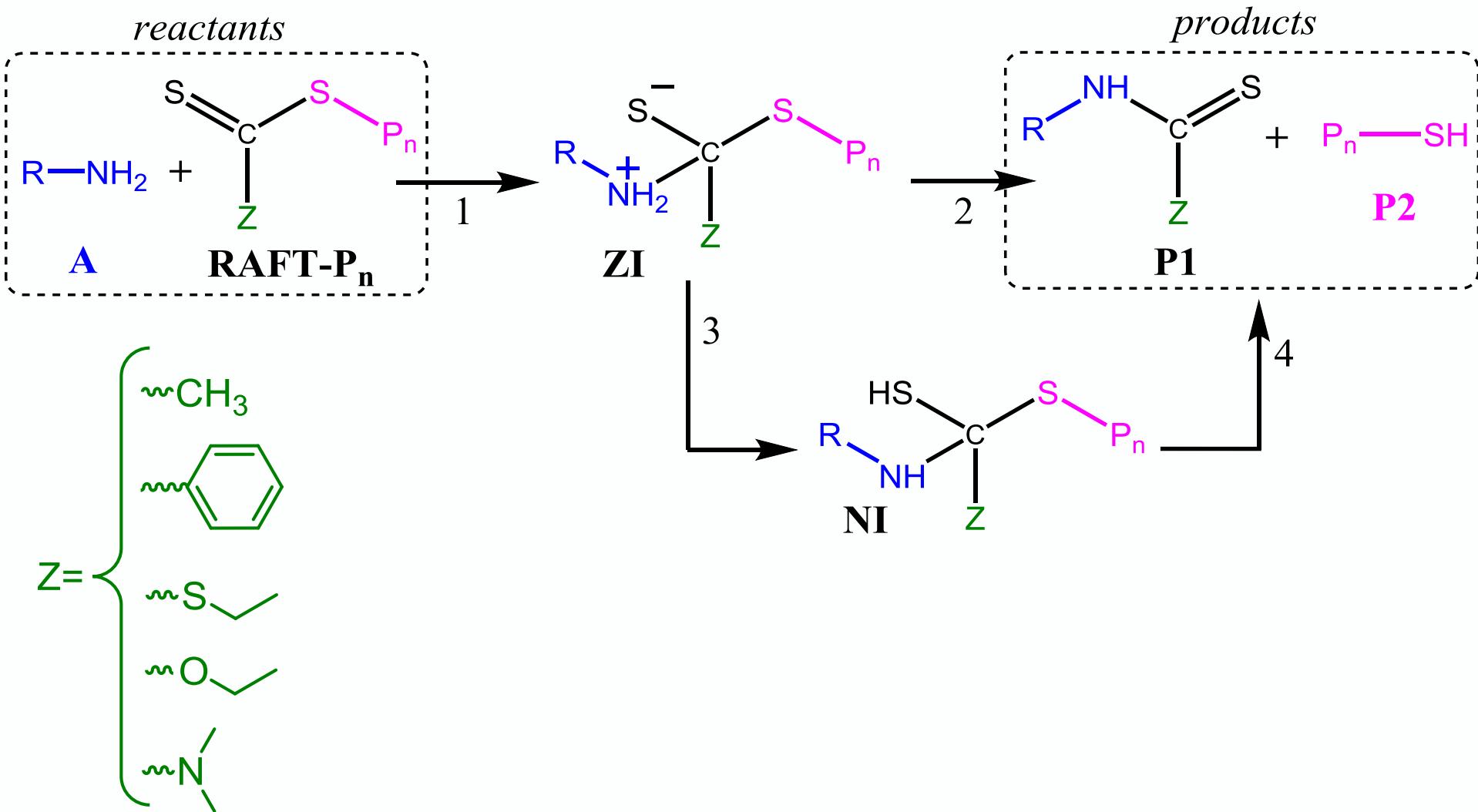
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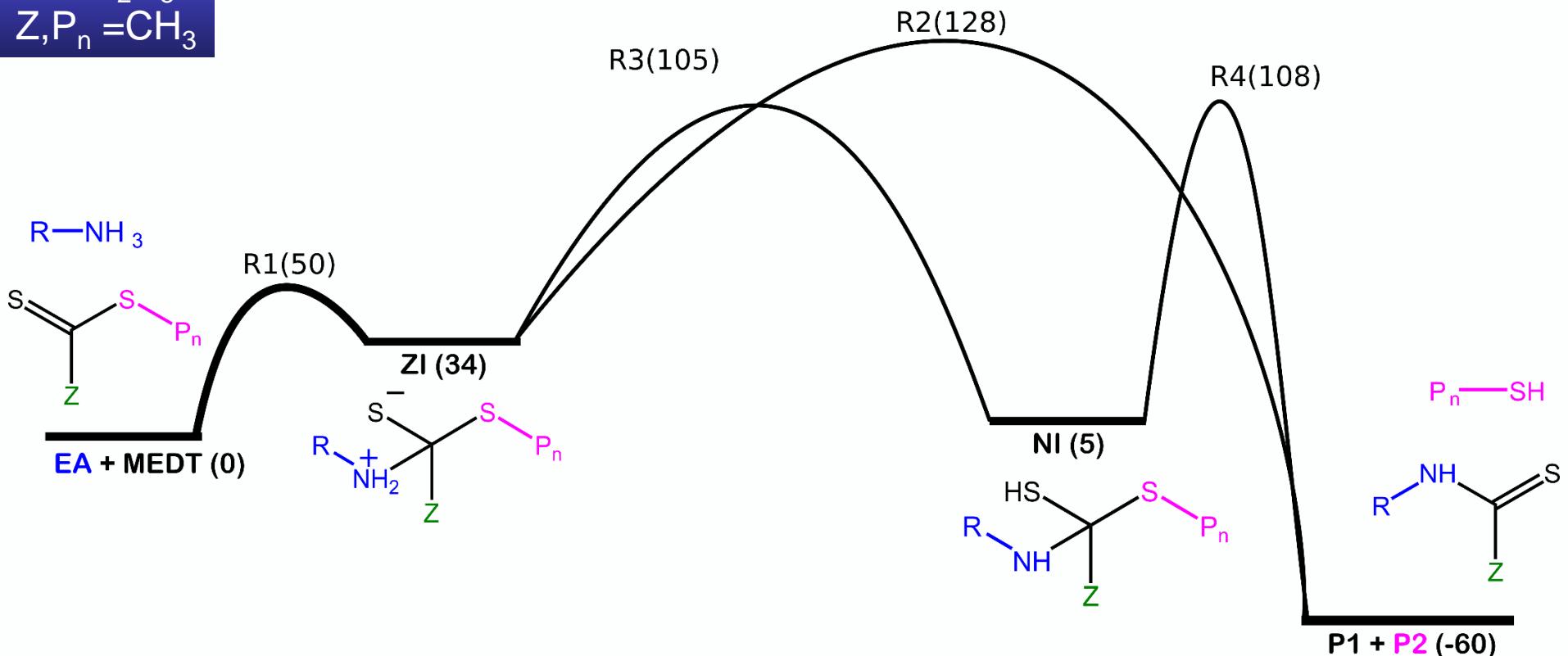


Aminolysis of RAFT agents in aprotic solvents: reaction mechanism



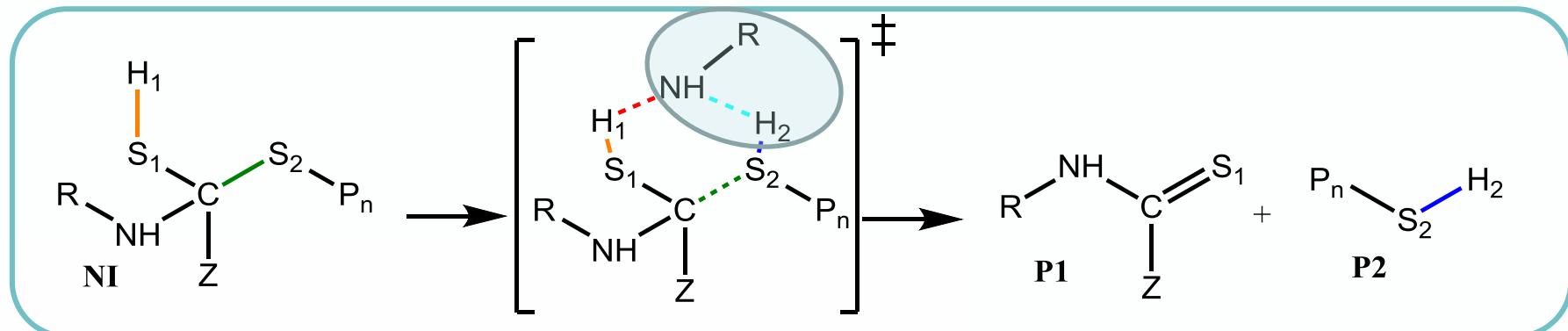
Gibbs Free Energy Diagram for EthylAmine (EA) + Methyl Ethane DiThioate (MEDT)

$R = C_2H_5$
 $Z, P_n = CH_3$

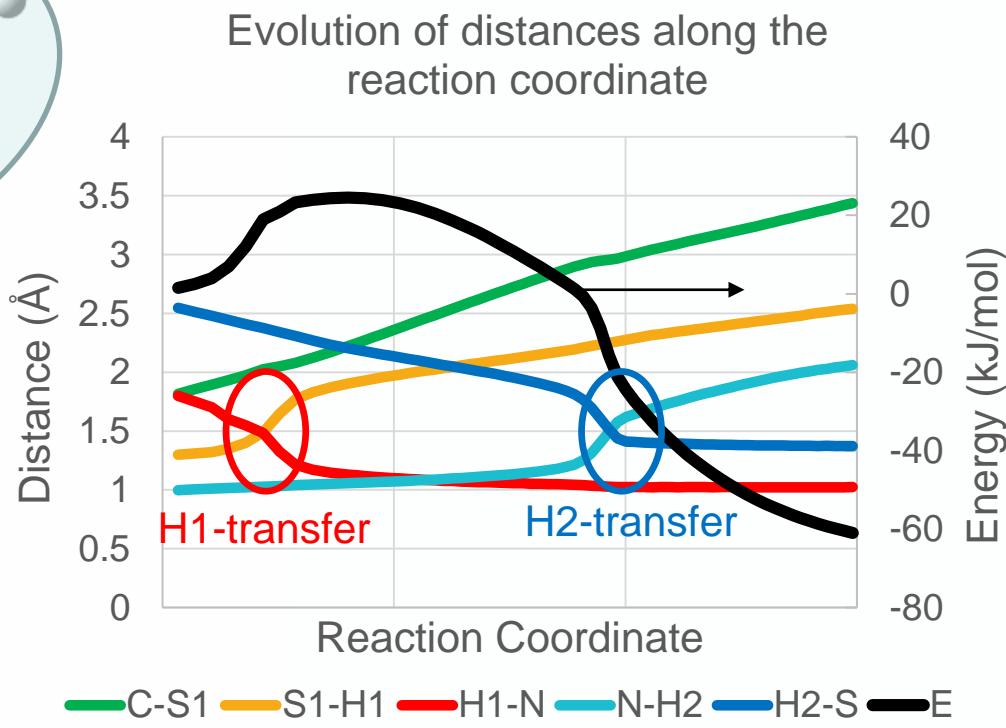
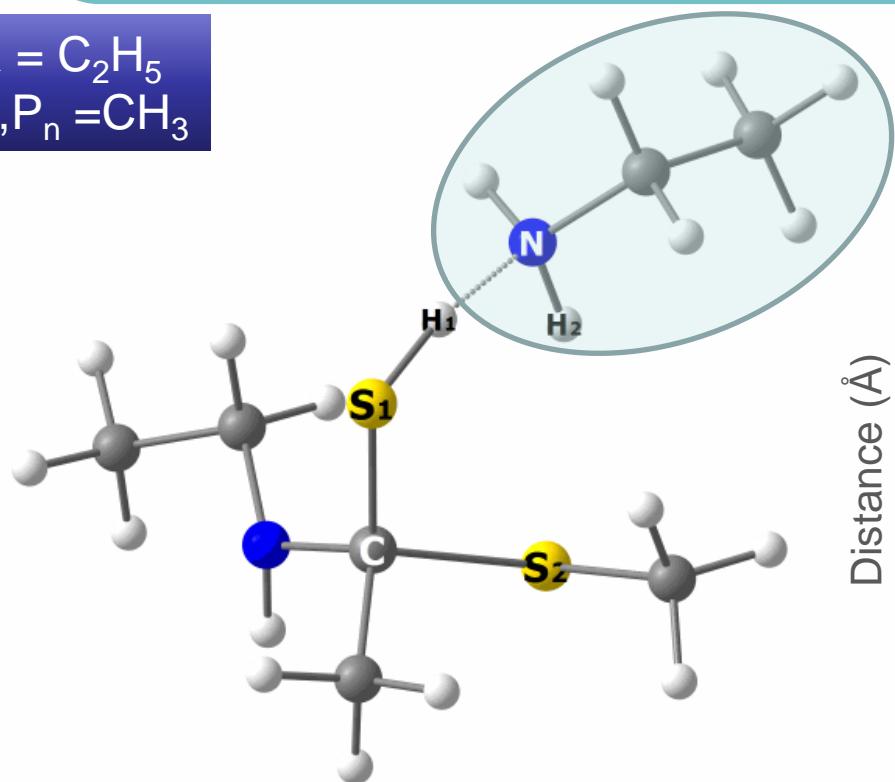


(Gibbs free energies in kJ mol⁻¹ at 298.15 K)

Amine assisted transition state are asynchronous and early

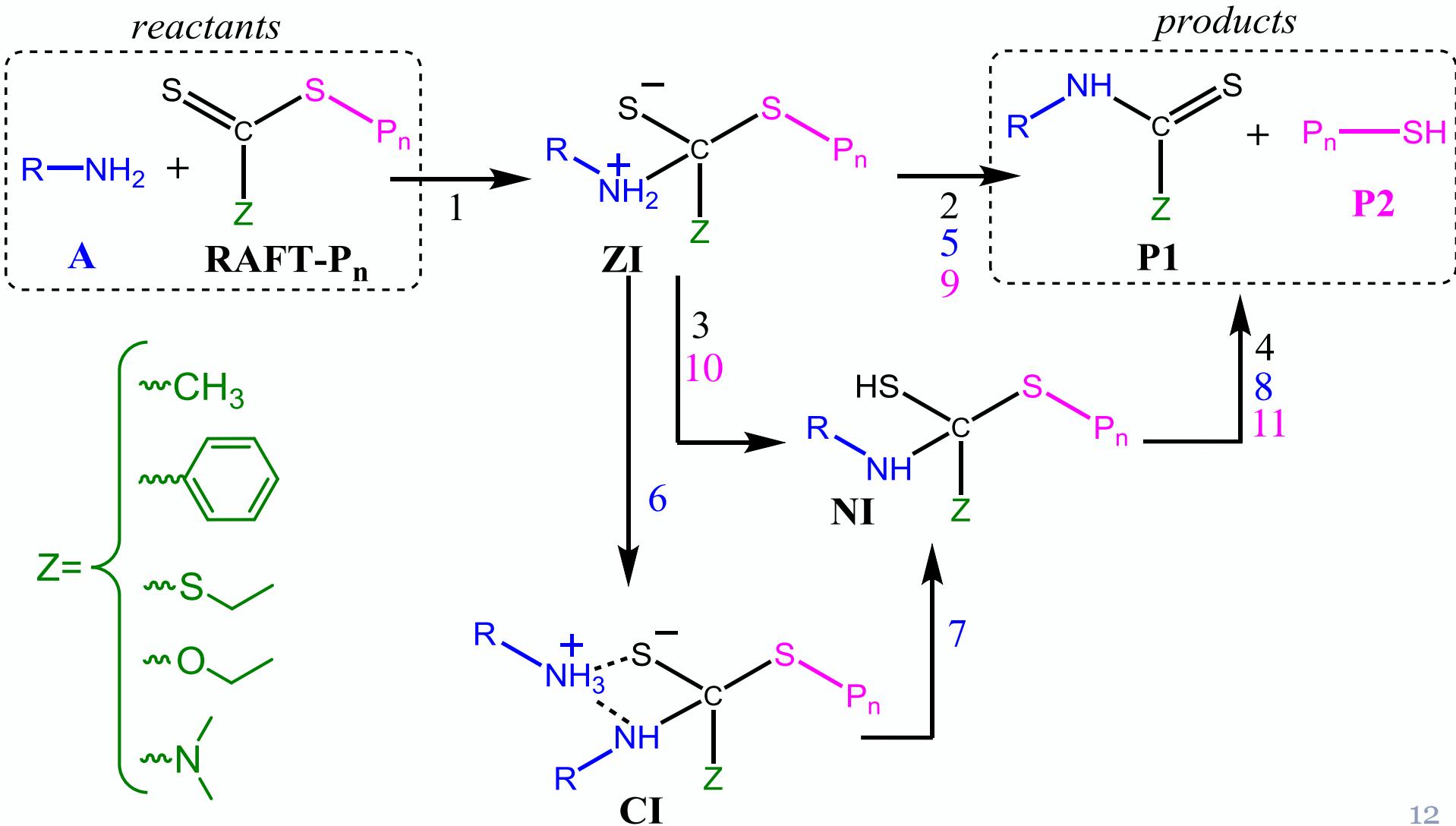


$$\begin{aligned} R &= C_2H_5 \\ Z, P_n &= CH_3 \end{aligned}$$

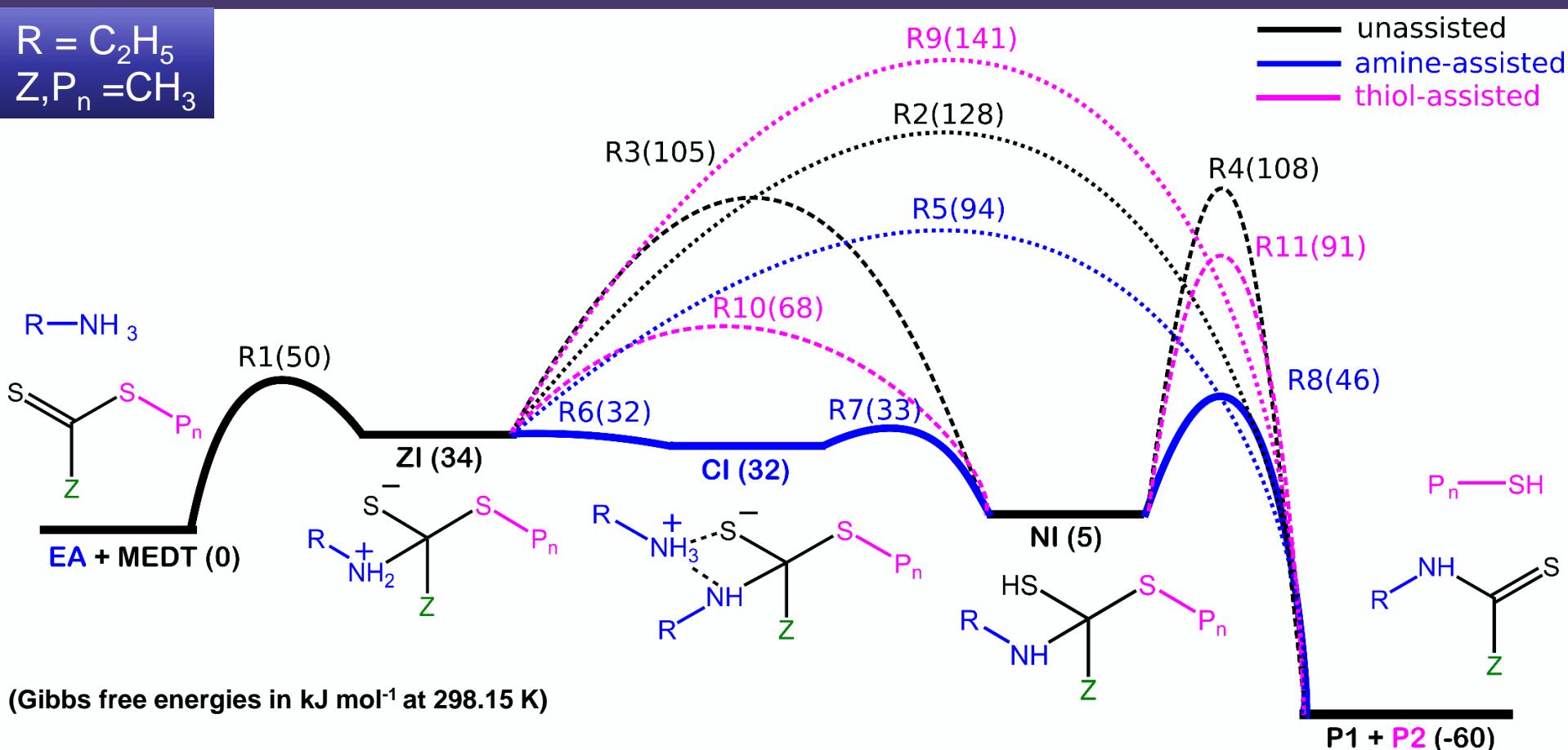


Aminolysis of RAFT agents in aprotic solvents: reaction mechanism

- Proton transfer in transition states can be assisted by **amines** and by **thiols**



Gibbs Free Energy Diagram for EthylAmine (EA) + Methyl Ethane DiThioate (MEDT)

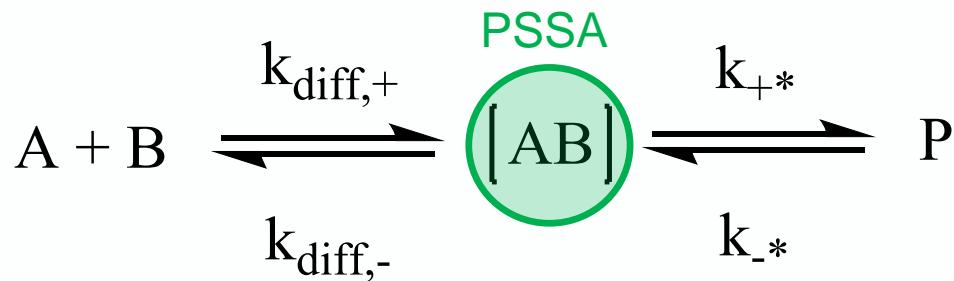


	R1	R2	R3	R4	R5	R6	R7	R8	R9	R10	R11
k_+	1.3E+04	2.3E-04	2.4E+00	4.3E-06	2.2E+02	6.2E+12	5.6E+12	3.4E+05	1.1E-06	7.8E+06	4.0E-03
k_-	1.3E+10	7.5E-21	1.5E-05	2.2E-17	7.2E-15	7.0E+12	7.6E+07	1.8E-06	3.6E-23	5.0E+01	2.1E-14

$(k_+ \text{ and } k_- \text{ in L mol}^{-1} \text{ s}^{-1} \text{ or } \text{s}^{-1})$

diffusional limitations become important!

The coupled encounter pair model to account for diffusion for TS 6 and 7



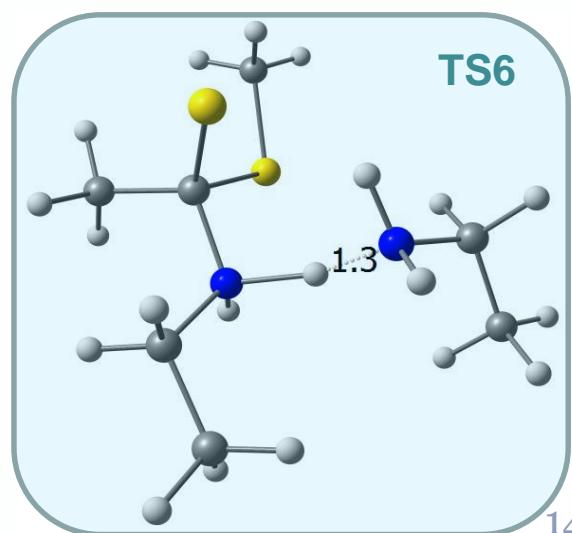
$$\frac{1}{k_{app,+}} = \frac{1}{k_+} + \frac{1}{k_{diff,+}}$$

$$\frac{1}{k_{app,-}} = \frac{1}{k_-} + \frac{K}{k_{diff,+}}$$

- Diffusion of A+B towards [AB] via the model of Smoluchowski: $k_{diff} = 4\pi N_A \sigma D_{AB}$

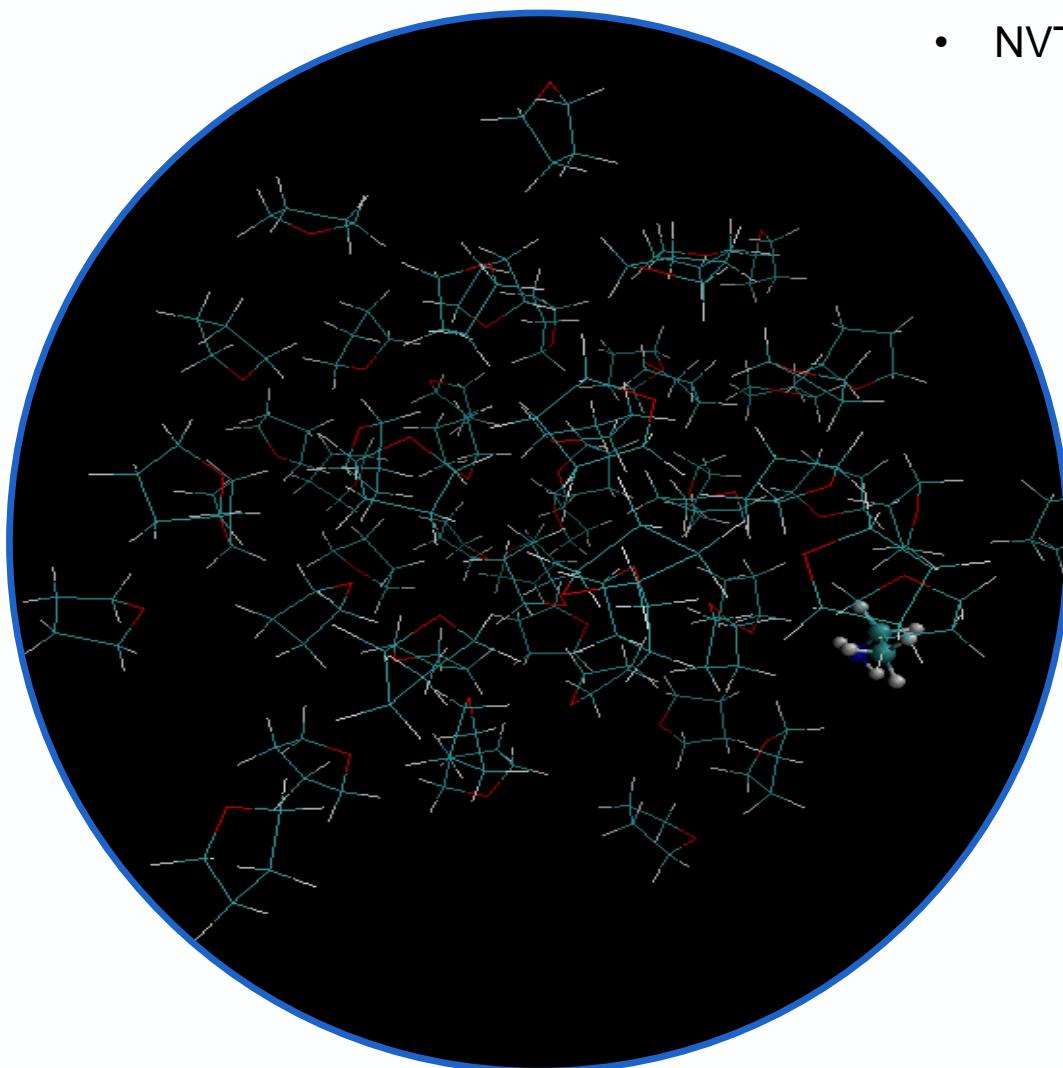
- σ = reaction distance: from ab initio TS geometries
- D_{AB} = mutual diffusivity coefficient^a
$$D_{AB} = \frac{D_A, D_B}{D_{solvent}}$$

MD



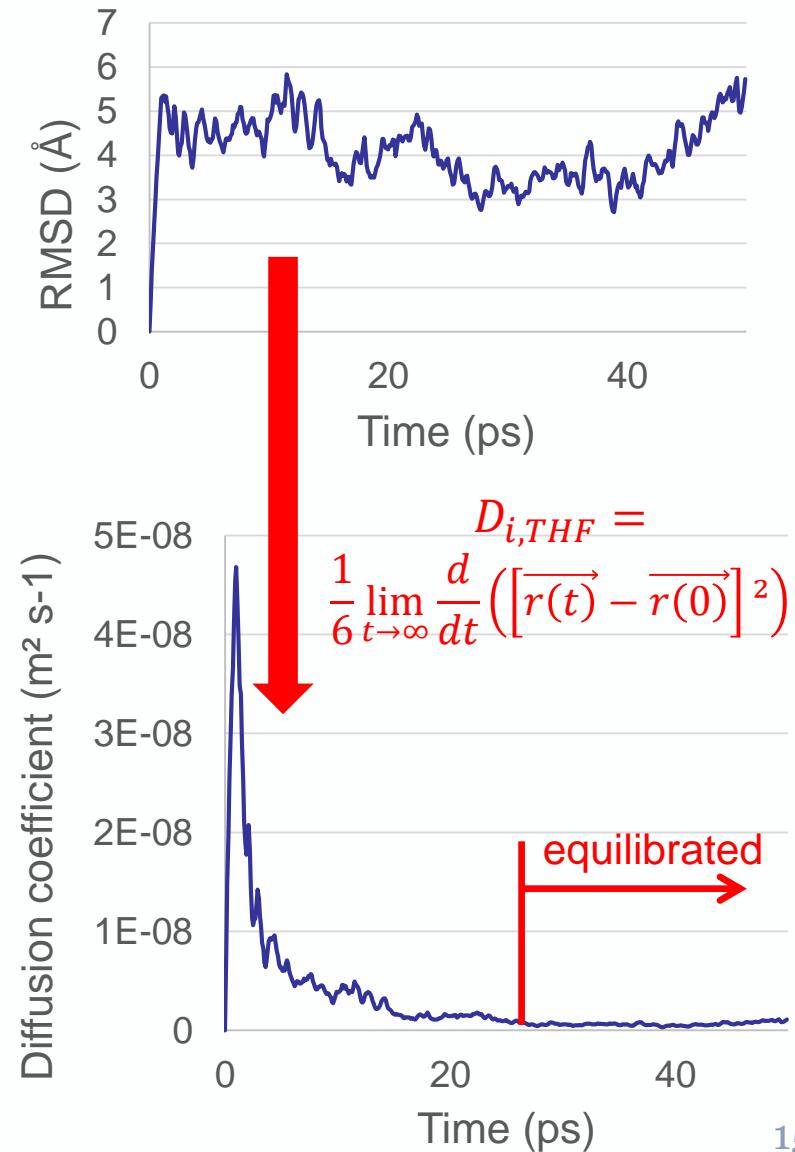
^a Liu et al. Ind Eng Chem Res 2011, 50, 4776.

Diffusivity coefficients based on molecular dynamics

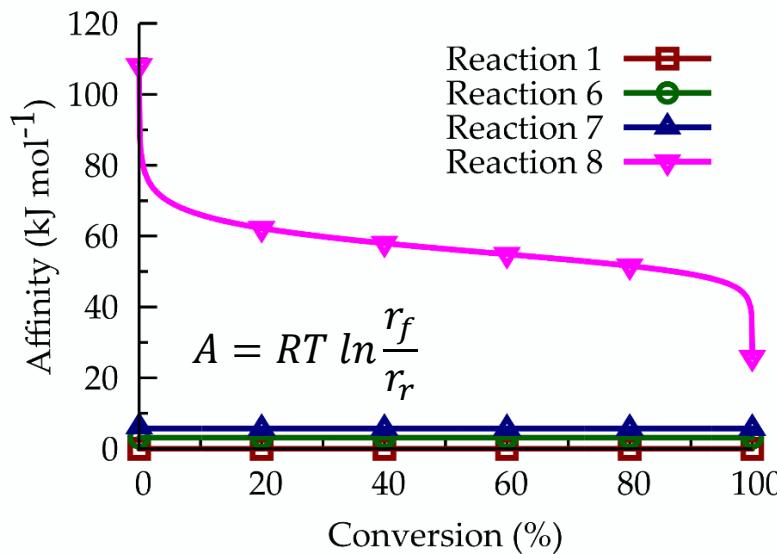
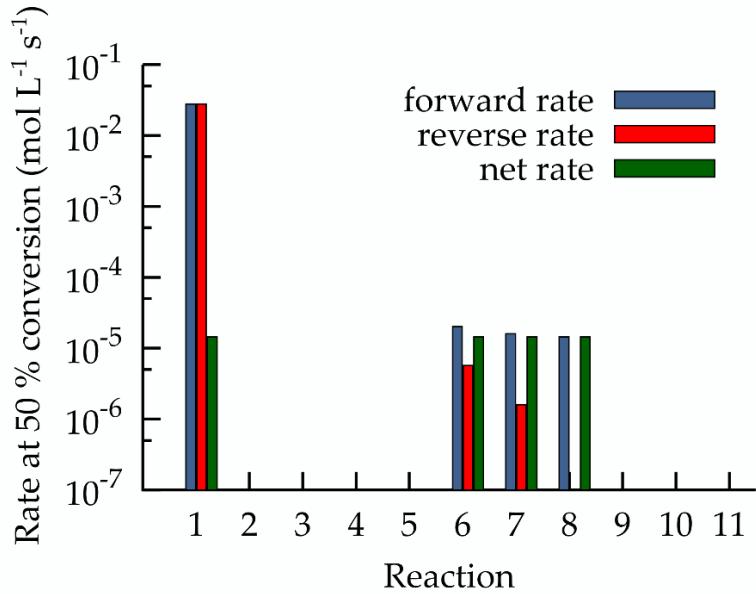


	k_+	k_{diff}	$k_{\text{app},+}$
R6	6.2E+12	2.1E+09	2.1E+09

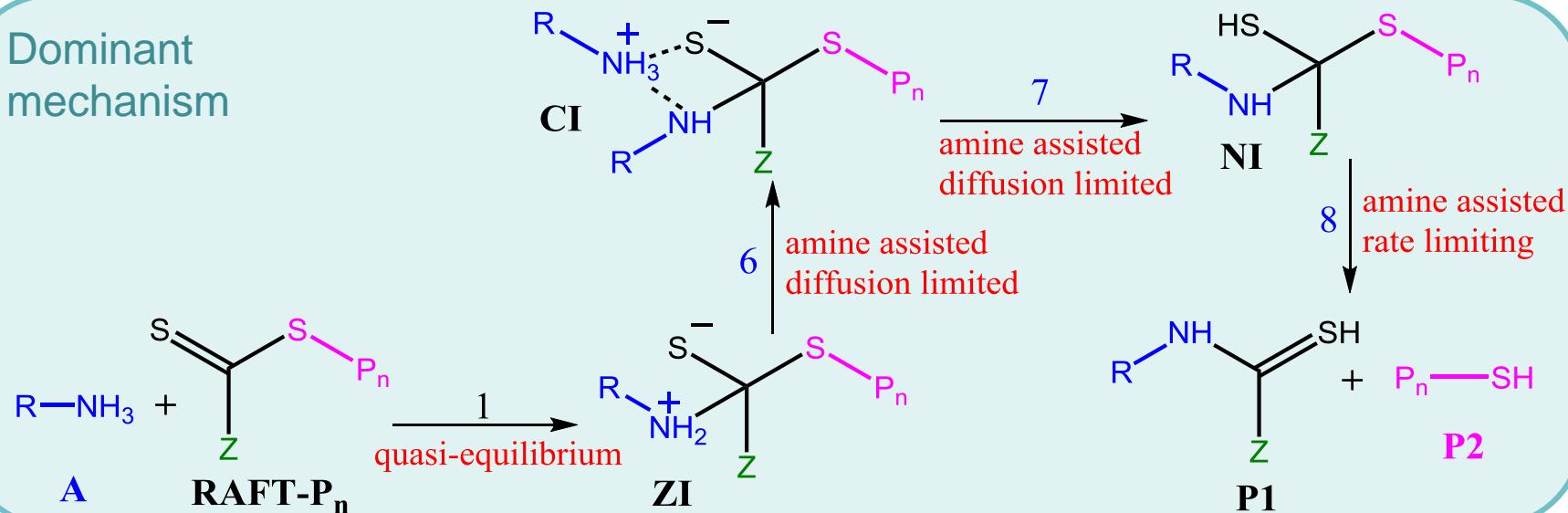
- NVT ensemble in 8 nm³ box for 50 picoseconds



Rate and affinity analysis reveal the dominant path and the nature of the elementary steps for the aminolysis of MEDT

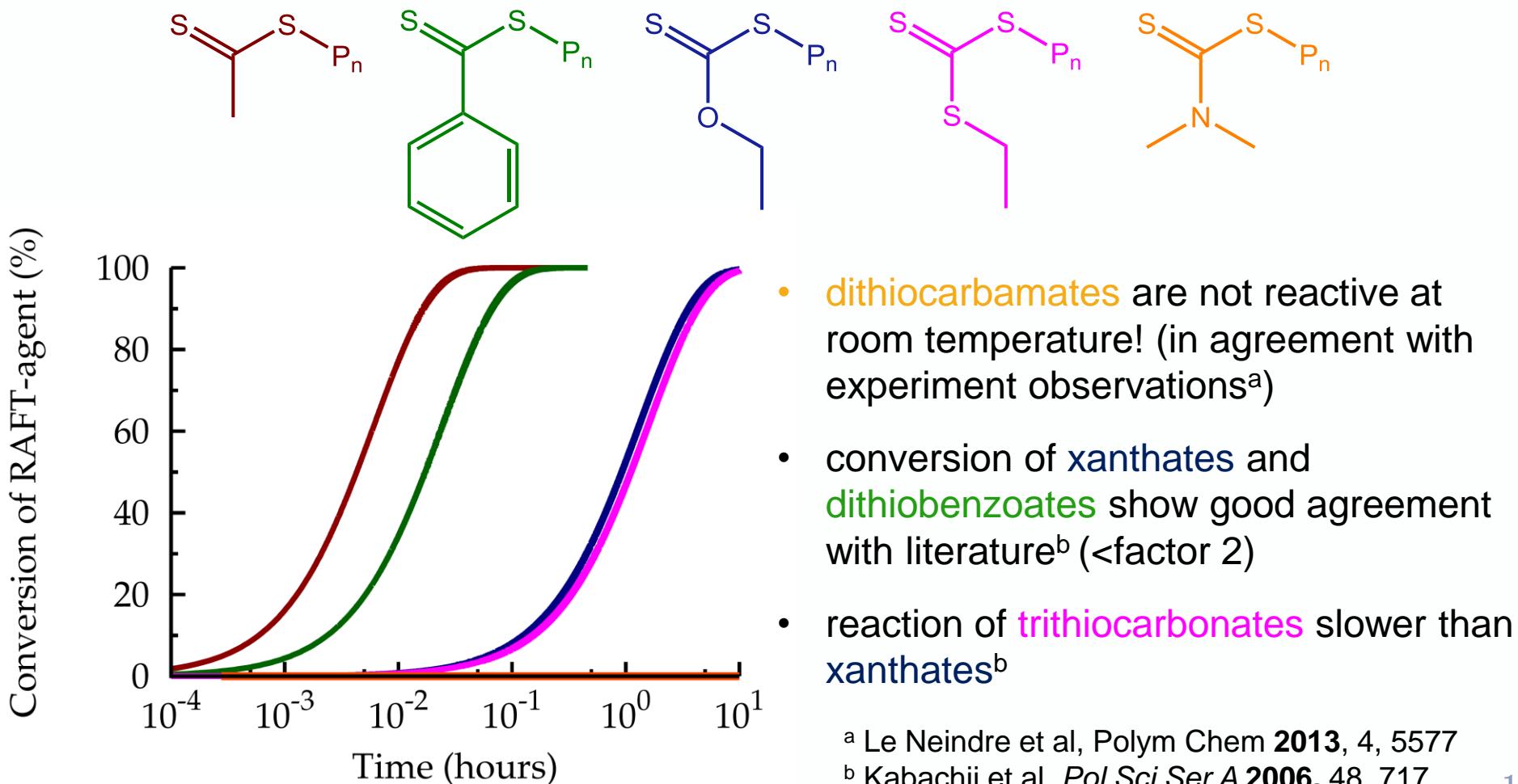


Dominant mechanism



Prediction of conversion profiles for other RAFT-agents

Reaction of 10^{-3} mol L⁻¹ RAFT-macromolecule with 5×10^{-3} mol L⁻¹ ethylamine in THF at 25 °C for **dithioates**, **thiobenzoates**, **xanthates**, **trithiocarbonates** and **dithiocarbamates**:



Conclusion: first principles techniques are a valuable tool to obtain reaction parameters for kinetic models

1. RAFT polymerization of styrene with a trithiocarbonate

- Calculation of **addition-fragmentation** rate coefficients
- Implementation in microkinetic model
 - conversions
 - chain lengths
 - dispersities

2. Aminolysis of RAFT-macromolecules

- Determining the **dominant mechanism** using ab initio based kinetic model
 - **quasi-equilibrated formation of a zwitterion**
 - **amine-assisted diffusion-limited proton transfer** over a complex intermediate towards a neutral intermediate
 - rate limiting amine-assisted breakdown of the neutral intermediate towards the product
- Simulation of conversion of range of RAFT agents
 - Reactivity: thioates > thiobenzoates > xanthates \geq trithiocarbonates $>>$ dithiocarbamates

Acknowledgements

Thanks to

- Nils De Rybel
- LCT colleagues

Funding



Questions?

