

Efficiency Comparison between the Steam Cycle and the Organic Rankine Cycle for Small Scale Power Generation

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Abstract

To generate electricity from biomass combustion heat, geothermal wells, recovered waste heat from internal combustion engines, gas turbines, or industrial processes, both the steam cycle and the organic Rankine cycle (ORC) are widely used. Both technologies are well established and can be found in comparable industrial applications. In this paper, we present a thermodynamic analysis and a comparative study of the cycle efficiency for a simplified steam cycle versus an ORC. We examine the application area of several working fluids based on their physical properties, considering some of the most commonly used organic fluids (R245fa, toluene, pentane, cyclopentane, and Solkatherm) and two silicon oils (MM and MDM). From computer simulations, we gain insight into the effect of several process parameters, such as the turbine inlet and condenser temperatures, the turbine isentropic efficiency, the vapor quality and pressure, and of the addition of a regenerator. We demonstrate that the thermal efficiency is primarily determined by the temperature level of the heat source and by the condenser conditions; and that the temperature profile of the heat source is the principal restricting factor for the evaporation temperature and pressure levels. Finally, we discuss some general and economic considerations relevant to the choice between a steam cycle and an ORC.

Keywords: organic Rankine cycle, steam cycle, waste heat recovery, cycle efficiency

1. Introduction

The past years have seen considerable growth in the generation of power from industrial waste heat. Due to the rising energy prices, even the recovery of low grade waste heat is becoming increasingly profitable. A frequently applied technology is the transformation of waste heat into electricity by means of a conventional steam turbine. This method utilizes the waste heat to produce steam which is then expanded over the turbine to generate electricity.

However, the obtainable electric efficiency of this power cycle is limited for the often low temperature levels of waste heat sources, which put a constraint on the related maximum superheating

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temperature and evaporation pressure of the generated steam. An alternative solution, based on the same technology, is the organic Rankine cycle (ORC). An ORC installation uses the same components as a conventional steam power plant, i.e., a heat exchanger, an evaporator, an expander and a condenser, to generate electric power, but its working fluid is an organic medium instead of water and steam. These organic fluids have some favorable properties compared to water and steam [1–4]. For instance, most of these fluids can be characterized as ‘dry’ fluids, implying that, at least theoretically, superheating of the vapor is not necessary. These fluids can be used at a much lower evaporation temperature – and pressure – than water in a conventional steam cycle, while still yielding competitive electric efficiencies or, at low temperatures, even showing superior performance.

Today, standard ORC modules are commercially available in the power range from a few kW up to 10 MW. The technology has been proven and successfully applied for several decades in geothermal plants and in solar and biomass fired combined heat and power (CHP) plants. Waste heat is abundantly available in industrial processes, often at low temperature levels and on small to moderate thermal power scales. Several studies of the working fluid [1–14] and of the optimization, control and economic aspects of ORCs [15–20] have appeared in the literature. The objective of this paper is to evaluate and compare the performance of an organic Rankine cycle with a classic steam cycle for small and low temperature heat sources. The paper is organized as follows. In Section 2, we discuss the influence of the working fluid properties. Then, in Section 3, we introduce the studied ORCs and steam cycles, list our assumptions and present our comparison results. The study is extended to situations that are characterized by a temperature profile of the heat source in Section 4. We present a list of arguments pro and contra the implementation of an ORC in Section 5 and give our main conclusions in Section 6.

2. Organic working fluids

To evaluate the characteristics of several organic fluids, we used the simulation software packages Fluidprop [21] and Cycle Tempo [22], developed at Technical University of Delft. We considered the following commonly used organic fluids: R245fa, toluene, pentane, cyclopentane, and Solkatherm, and the silicon oils MM and MDM. In Table 1, we reproduce some thermophysical properties for these fluids and for water.

From Table 1 it follows that the critical pressure and, consequently, also the operating pressure at the inlet of the turbine in a (subcritical) ORC system are much lower than in the case of a classical steam cycle. Although steam turbines exist that operate in a low pressure steam regime, the thermal efficiency of a steam cycle also decreases with lower turbine pressure.

All of the above organic fluids are dry fluids. Dry fluids are characterized by a positive slope of the saturated vapor curve in the temperature-entropy (T - s) diagram. Water, on the other hand, is a ‘wet’ fluid, with a negative slope. In Figure 1, the T - s diagram of the silicon oil MM is represented. Dry fluids do not require superheating and saturated vapor can thus be supplied to an ORC expander. After expansion, the working fluid remains in the superheated vapor region. By comparison, in a steam cycle, the steam is usually superheated to avoid moisture formation in the final turbine stages, which would otherwise affect the performance and durability of the steam turbine.

Fluid	Formula/name	MW [kg/mol]	T_{crit} [°C]	p_{crit} [bar]	BP [°C]	E_{evap} [kJ/kg]
Water	H ₂ O	0.018	373.95	220.64	100.0	2257.5
Toluene	C ₇ H ₈	0.092	318.65	41.06	110.7	365.0
R245fa	C ₃ H ₃ F ₅	0.134	154.05	36.40	14.8	195.6
n-pentane	C ₅ H ₁₂	0.072	196.55	33.68	36.2	361.8
cyclopentane	C ₅ H ₁₀	0.070	238.55	45.10	49.4	391.7
Solkatherm	solkatherm	0.185	177.55	28.49	35.5	138.1
OMTS	MDM	0.237	290.98	14.15	152.7	153.0
HMDS	MM	0.162	245.51	19.51	100.4	195.8

Table 1: Thermophysical properties of the fluids in this study. Listed are the chemical formula or common name, the molar weight, the critical temperature and pressure, the boiling point, and the evaporation heat.

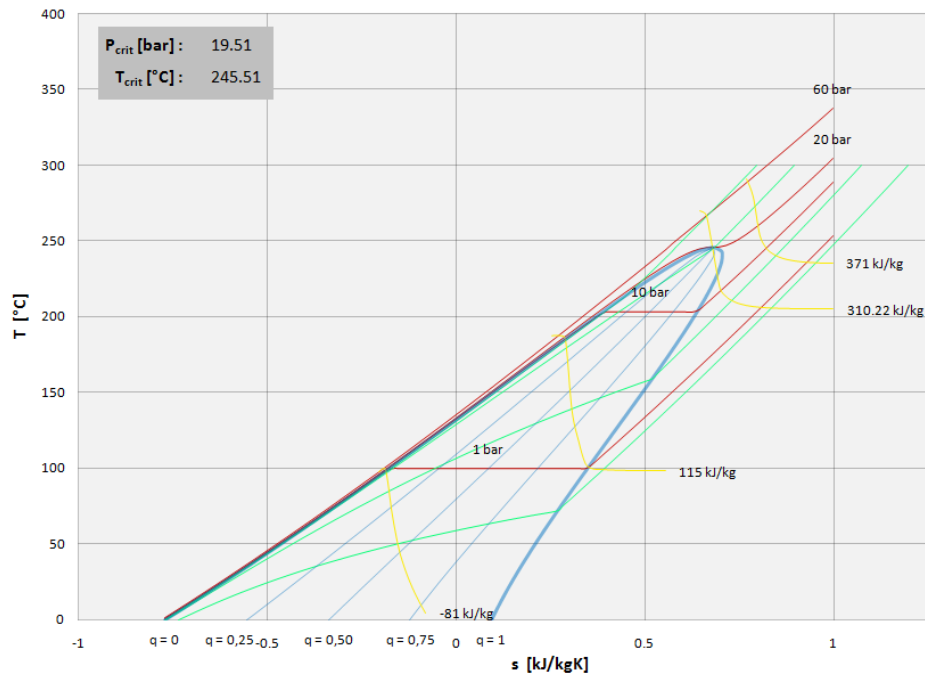


Figure 1: $T-s$ diagram of the silicon oil MM. As an example of a dry fluid, the slope of the saturated vapor curve (blue line) is positive.

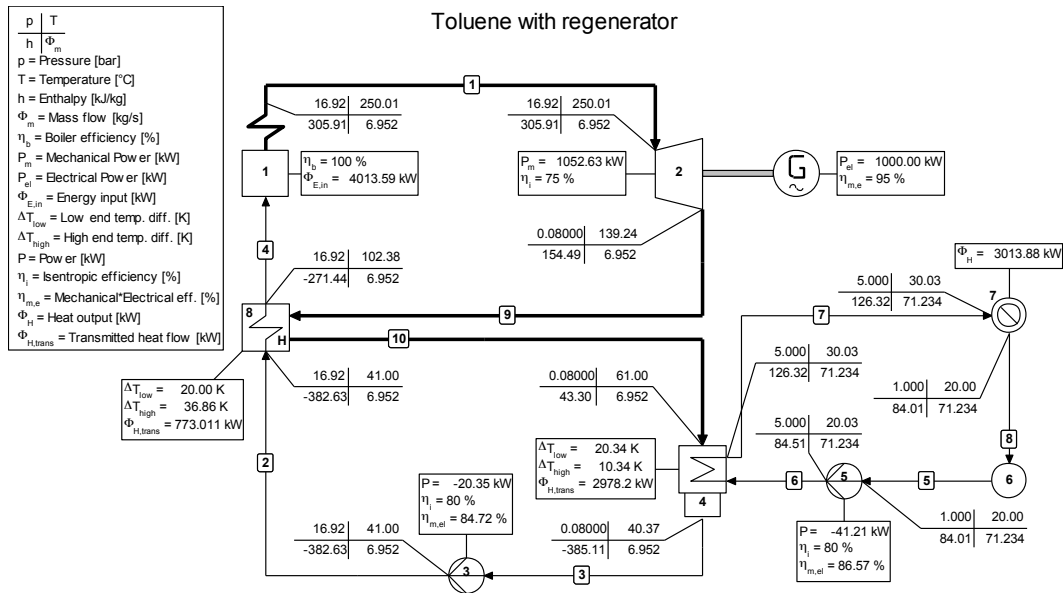


Figure 2: Cycle diagram of a toluene based ORC, equipped with a regenerator.

As a general rule, a fluid with a higher boiling point has a lower condensation pressure at ambient temperature, and, after expansion, a lower density and a higher specific volume. For water and steam in particular, large diameters of the final turbine stages and a voluminous condenser are expected. Organic fluids have densities that are an order of ten times higher than the density of water/steam and therefore require smaller turbine diameters. However, the evaporation heat of organic fluids is also about ten times smaller, which corresponds to higher mass flows in the ORC, and hence much bigger feed pumps.

In short, the thermophysical properties of the working fluid have an effect on the design and complexity of the heat exchangers, the turbine and the condenser, and need to be taken into account during the economic analysis and comparison.

3. ORC versus steam cycle

3.1. Organic Rankine cycle

In Figure 2, we reproduce the cycle diagram, made with Cycle Tempo [22], of an ORC with toluene as the working fluid and with a regenerator. The corresponding thermodynamic cycle is represented by the T - s diagram in Figure 3. A regenerator is often used to reach a higher cycle efficiency. After expansion, the organic fluid remains considerably superheated above the condenser temperature. This sensible heat can be exploited to preheat the organic liquid in a heat exchanger after the condenser stage. The higher the evaporation temperature, the higher the effect of a regenerator on the cycle efficiency. In Figure 4, this influence of a regenerator on the cycle efficiency is made apparent for the specific case of an ORC based on the silicon oil MM as a working fluid, assuming the parameters listed in Table 2.

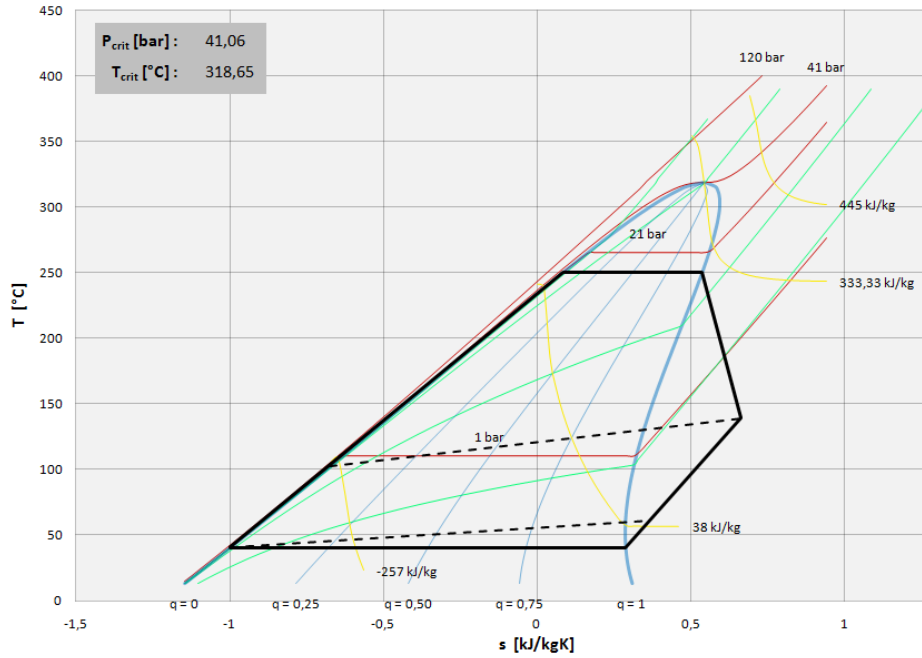


Figure 3: T - s diagram of toluene and the ORC cycle steps (black lines) corresponding to the specifications in Figure 2.

Parameter	Unit	Value
Condenser temperature	[°C]	40
Isentropic efficiency turbine	[%]	75
Isentropic efficiency pump	[%]	80
Electromechanical efficiency pump	[%]	90
Electromechanical efficiency generator	[%]	90
Superheating temperature ORC	[°C]	5
Regenerator pinch	[°C]	15
Inlet turbine ORC		Saturated
Inlet turbine steam		Superheated
Vapor quality steam at outlet turbine	[%]	90

Table 2: Cycle parameters used in the analysis of ORCs and the steam cycle.

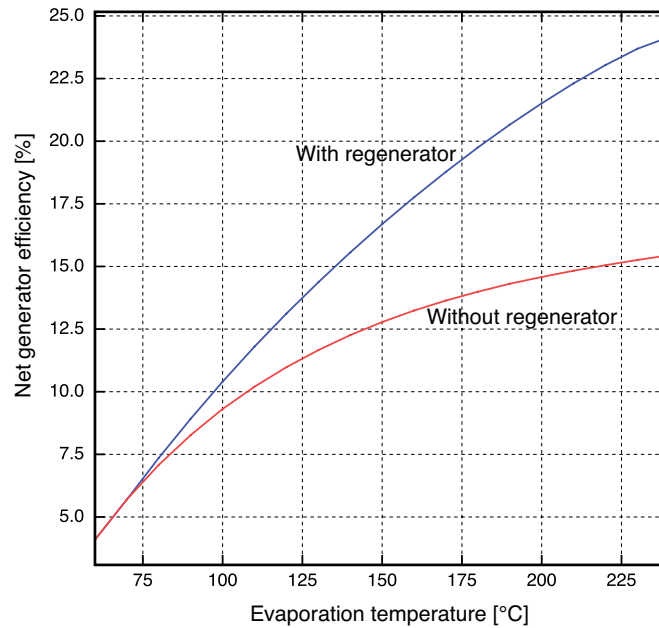


Figure 4: Net generator efficiency as a function of the evaporation temperature for an MM (silicon oil) based ORC, with and without regenerator. Parameters as in Table 2.

3.2. Simplified steam cycle

In Figure 5, we show the cycle diagram of the simplified steam cycle without deaerator that we choose as the reference system in our comparison with ORC installations. Although this diagram appears very similar to the one of an ORC without regenerator, there is one significant difference. Whereas saturated vapor can be applied in ORCs, a classic steam cycle commonly works with superheated steam. Steam turbines that *can* manage saturated steam typically have very poor isentropic efficiencies.

The inlet and outlet conditions of a steam turbine are correlated via the isentropic efficiency of the turbine. As a consequence, to achieve a prescribed vapor quality at the turbine outlet, the correspondence between the evaporation pressure and the minimum superheating temperature must be taken into account.

In this study, we compare the simplified steam cycle with an ORC, with and without a regenerator. In a follow-up study, the model of the steam cycle will be refined by the inclusion of a deaerator, which has a minor positive influence on the cycle efficiency.

3.3. Assumptions

The assumptions mentioned in the presentation above of the ORC and the steam cycle, apply to the remainder of this paper. The performance of the cycles is evaluated assuming stationary conditions of all the components, with parameters mentioned in Table 2. In addition, we assume that mass and energy are conserved in each cycle component, and that no pressure and energy losses occur. To enable the comparison between cycles based on wet and dry fluids, the optimal

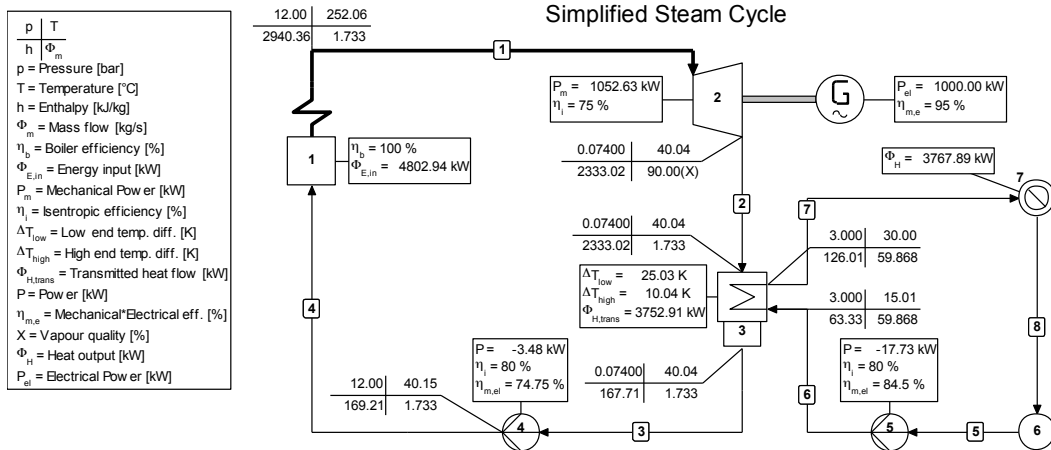


Figure 5: Cycle diagram of the simplified steam cycle.

cycle determined by the predefined set of temperature levels of the heat source and the condenser is considered for each case. In this part of the study, we assume that the heat source is at a constant temperature level that also defines the turbine's inlet temperature. Hence, only cycles with identical turbine inlet temperatures and condenser temperatures are compared. Later in this paper, we extend our analysis by considering a predefined temperature *profile* of the heat source, together with an optimized turbine inlet pressure to maximally exploit the available heat.

3.4. Results

In Figure 6, we plot the achieved cycle efficiency as a function of the turbine inlet temperature for all considered fluids. We note that for inlet temperatures below circa 130 °C it is impossible for the considered steam cycle to reach the preset turbine outlet conditions. Based on these results, we can state that: (i) ORCs display a superior performance compared to the simplified steam cycle, assuming equal temperatures at the turbine inlet; (ii) of the working fluids considered, the best ORC performance is achieved by toluene; and (iii) the application area of ORCs based on conventional working fluids, without superheating, is confined to temperatures below 300 °C.

3.5. Additional remarks and considerations

We conclude this part of the study with some additional remarks and considerations. In the field, there is a variety of expanders (e.g., turbine, screw expander) found in ORCs. Although isentropic efficiencies of 85% to 90% are attainable for turbines with a dedicated design, in practice, the isentropic efficiencies of small scale steam turbines, for low pressure applications, and with limited superheating temperature, are found to be lower than 75%. The efficiencies of commercially available ORCs may also fall short of our predictions, depending on the validity of our assumptions, such as for the pressures and temperatures at the inlet and outlet of the turbine and for the isentropic efficiency.

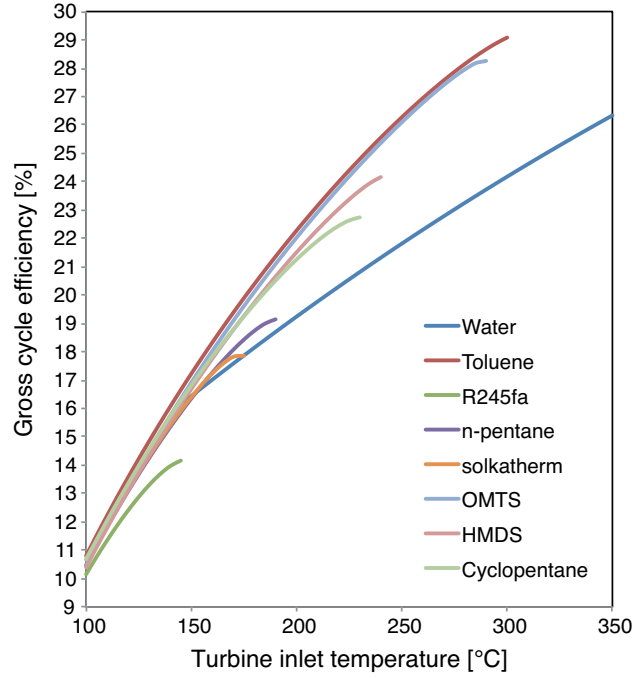


Figure 6: Cycle efficiency as a function of the turbine inlet temperature for all considered fluids.

4. Influence of the temperature profile of the heat source

In reality, the temperature of a waste heat source does not remain at a constant level, but has a given temperature profile. This profile defines the thermal power P_{th} available between the inlet and outlet temperatures, and is dependent on the mass flow and medium type of the heat source. The closer the heating curves of the cycle (preheating, evaporation, and superheating) fit this temperature profile, the more efficiently the waste heat will be transformed by the ORC or steam cycle. In this part of the paper, we report our simulations for an arbitrary temperature profile of the waste heat source. In Table 3, we list the parameters assumed for this part of the study.

Design calculations of a heat exchanger, used in the recovery of industrial waste heat, lie beyond the scope of this study. Nevertheless, the effectiveness of the heat exchanger is taken into account by defining a ‘pinch line’ with an offset of 20 °C with respect to the temperature profile of the waste heat source. The attainable superheating temperature for the simplified steam cycle is then a function of the evaporation pressure p_{evap} , the vapor quality q , the condenser temperature T_{cond} , and the isentropic efficiency η_i of turbine, and is bounded by this pinch line.

In Table 4, we present our results for the gross ($P_{gen,bto}$) and net generator power ($P_{gen,nto}$) and the cycle efficiency η . The net generator power is given by $P_{gen,nto} = P_{gen,bto} - P_{pump}$, with P_{pump} the pump power. Depending on p_{evap} and the superheating temperature T_{sup} , only a fraction $P_{th, reco}$ of the thermal energy of the heat source can be recovered. In Figure 7, the corresponding heating profiles for the cases of Table 4 are reproduced. This figure makes visible that the ORC pinch point is determined by the temperature after the regenerator. For the steam cycle, the selected evaporation pressure and superheating temperature are the constraining variables. Since the evaporation

Waste heat source		Simplified steam cycle	
T -profile	350-120 °C	T_{cond}	40 °C
P_{th}	3000 kW _{th}	η_i turbine	70-80%
pinch	20 °C	q	93%
ORC		Components	
medium	HMDS	η_i pump	80%
ΔT_{sup}	10 °C	$\eta_{m,e}$ pump	90%
T_{cond}	40 °C	$\eta_{m,e}$ generator	90%
η_i turbine	70-80%		

Table 3: Parameters used in the analysis of ORCs and the steam cycle in the case where the waste heat source is characterized by a temperature profile. P_{th} is the thermal power of the heat source, T_{cond} is the condenser temperature, η_i signify the isentropic efficiencies of the said components, $\eta_{m,e}$ the electromechanical efficiencies, q is the vapor quality, and ΔT_{sup} is the superheating temperature. Note that the latter in a steam cycle is a function of the evaporation pressure, the vapor quality, the condenser temperature, and the isentropic efficiency of turbine.

Case	η_i turb [%]	p_{evap} [bar]	T_{sup} [°C]	$\eta_{cycle,bto}$ [%]	$\eta_{cycle,nto}$ [%]	$P_{gen,bto}$ [kW _e]	$P_{gen,nto}$ [kW _e]	$P_{th,reco}$ [kW _{th}]
O ₁	70	14.0	234	20.4	19.7	506	488	2479
O ₂	70	17.6	248	21.3	20.4	509	487	2388
O_{opt}	70	14.9	239	20.7	19.8	513	492	2478
S ₁	70	6.0	219	16.1	16.0	440	439	2737
S ₂	70	12.0	272	18.5	18.5	442	441	2386
S ₃	70	18.0	305	19.9	19.9	426	424	2134
S_{opt}	70	7.9	320	17.6	17.6	454	453	2572
O ₃	80	14.0	234	22.6	21.9	574	556	2540
O ₄	80	17.6	248	23.6	22.7	578	556	2452
O_{opt}	80	16.3	244	23.3	22.4	583	561	2505
S ₄	80	6.0	267	18.7	18.7	509	508	2715
S ₅	80	12.0	330	21.6	21.5	509	508	2357
S_{opt}	80	7.9	320	20.2	20.1	519	518	2571

Table 4: Gross and net cycle efficiencies, $\eta_{cycle,bto}$ and $\eta_{cycle,nto}$, and gross and net generator power, $P_{gen,bto}$ and $P_{gen,nto}$, of MM based ORCs (O₁, O₂, O₃, O₄) and steam cycles (S₁, S₂, S₃, S₄, S₅) with a temperature profile and parameters as indicated in Table 3. Variables are the isentropic turbine efficiency η_i , the evaporation pressure p_{evap} , and the superheating temperature T_{sup} . Also listed is the recovered thermal heat $P_{th,reco}$. O_{opt} and S_{opt} represent cases of MM based ORCs and steam cycles, respectively, with optimized variables to obtain the highest possible net generator power under the conditions of Table 3.

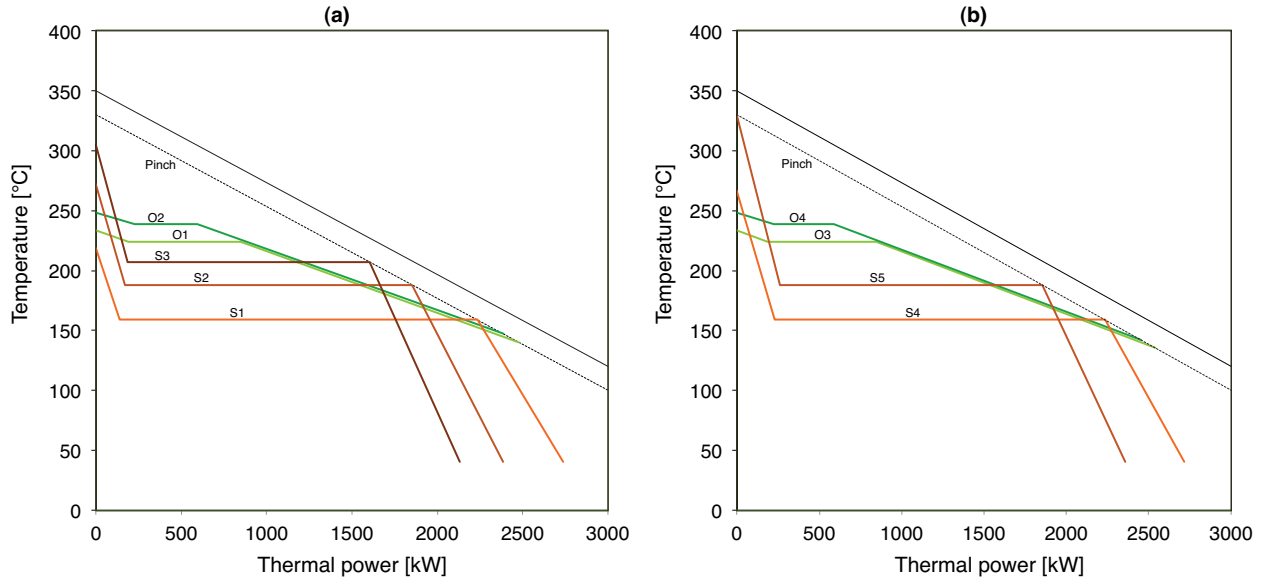


Figure 7: Heating profiles for the cases of Table 4. In (a) the isentropic turbine efficiency is 70% for all cases, in (b) it is 80%.

heat E_{evap} for organic fluids is much smaller than for water, a higher evaporation temperature can be selected and therefore less thermal energy is required at higher temperature levels in an ORC. The result is a higher cycle efficiency and a 10 to 15% increase in electric power generation for the ORCs presented in this case study.

Also included in Table 4 are our results for the optimization with respect to the net generator power of an ORC (O_{opt}) and a steam cycle (S_{opt}), for isentropic turbine efficiencies of 70% and 80%, and under the conditions of Table 3.

5. Selection arguments

Based on our research, other studies, extensive experience and shared knowledge with constructors, suppliers and operators of both steam cycle and ORC based power plants, we list some general arguments that we think should be considered when faced with the choice between a steam cycle and an ORC. These factors should then be included in an investment, maintenance and exploitation plan.

The following are arguments in favor of an ORC implementation.

- Most organic fluids used in ORC installations are dry fluids that do not require superheating. Important factors in the total installation cost are the design and the dimensions of the heat exchangers (i.e., preheater, evaporator, and superheater) for the waste heat recovery. Superheater dimensions are usually large because of the lower heat transfer per surface unit for a gaseous medium.
- The isentropic efficiency of a turbine varies with its power range and its design. In general,

ORC expanders with a dedicated design have a higher efficiency than small scale steam turbines in the same power range.

- There is no need for meticulous process water treatment and control, nor for a deaerator.
- The installation is less complex, which is desirable when starting from a green field or when there is no steam network with appropriate facilities already present on the site.
- Maintenance costs are very low and the availability is high.
- The operation is very simple, usually only involving start and stop buttons.
- The behavior and efficiency under partial load is good.
- The system pressure is much lower and the applicable safety legislation is less stringent.
- A qualified operator is not required.
- Electrical outputs of less than 1 kW_e are available. Small scale steam turbines (e.g. 10 kW_e) exist, but steam turbines only become profitable at higher power outputs (above 1 MW_e).

The next arguments support the choice for a steam cycle.

- Water as a working fluid is cheap and abundant, while ORC fluids can be very expensive or their use restricted by environmental arguments. Large on-site steam networks, which require high amounts of working fluid (steam), are feasible.
- The flexibility of the power/heat ratio – important for biomass fired CHPs – can be higher due to the possibility to add steam extraction points on the turbine or by using a back pressure steam turbine.
- Direct heating and evaporation is possible in (waste) heat recovery heat exchangers, therefore there is no need for an intermediate (thermal oil) circuit.
- Some standard ORCs are designed to work with an intermediate thermal oil circuit to transport the waste heat to the ORC preheater and evaporator. This technique requires less ORC fluid, but tends to make the installation more complex and expensive, and results in an additional temperature drop. Furthermore, some fire accidents with thermal oil circuits are known.

6. Conclusions

The main conclusions that we draw from this study are the following. First, ORCs can function in combination with low temperature heat sources, characterized by low to moderate evaporation pressure, and still achieve better performances than steam cycles. Next, ORCs require larger feed pumps, because of their inherent higher mass flow, which in turn affects the net electric power. And finally, the heating curves of ORCs can be better matched to the temperature profiles of waste heat sources, resulting in higher cycle efficiencies and higher thermal power recovery ratios.

7. Acknowledgements

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References

- [1] P. J. Mago, L. M. Chamra, K. Srinivasan, C. Somayaji, An examination of regenerative organic Rankine cycles using dry fluids, *Applied Thermal Engineering* 28 (2008) 998–1007.
- [2] T. Hung, Waste heat recovery of organic Rankine cycle using dry fluids, *Energy Conversion and Management* 42 (2001) 539–553.
- [3] B. Liu, K. Chien, and C. Wang, Effect of working fluids on organic Rankine cycle for waste heat recovery, *Energy* 29 (2004) 1207–1217.
- [4] G. Angelino and P. Colonna di Paliano, Multi-component Working Fluids For Organic Rankine Cycles (ORCs), *Energy* 23 (1998) 449–463.
- [5] S. Vijayaraghavan, D. Y. Goswami, Organic Working Fluids for a Combined Power and Cooling Cycle, *Journal of Energy Resources Technology* 127 (2) (2005) 125–130.
- [6] B. Saleh, G. Koglbauer, M. Wendland, J. Fischer, Working fluids for low-temperature organic Rankine cycles, *Energy* 32 (2007) 1210–1221.
- [7] U. Drescher, D. Brüggemann, Fluid selection for the Organic Rankine Cycle (ORC) in biomass power and heat plants, *Applied Thermal Engineering* 27 (2007) 223–228.
- [8] B. F. Tchanche, G. Papadakis, G. Lambrinos, A. Frangoudakis, Fluid selection for a low-temperature solar organic Rankine cycle, *Applied Thermal Engineering* 29 (2009) 2468–2476.
- [9] G. Kosmadakis, D. Manolakos, S. Kyritsis, G. Papadakis, Comparative thermodynamic study of refrigerants to select the best for use in the high-temperature stage of a two-stage organic Rankine cycle for RO desalination, *Desalination* 243 (2009) 74–94.
- [10] F. Heberle, D. Brüggemann, Exergy based fluid selection for a geothermal Organic Rankine Cycle for combined heat and power generation, *Applied Thermal Engineering* 30 (2010) 1326–1332.
- [11] A. A. Lakew, O. Bolland, Working fluids for low-temperature heat source, *Applied Thermal Engineering* 30 (2010) 1262–1268.
- [12] W. C. Andersen, T. J. Bruno, Rapid Screening of Fluids for Chemical Stability in Organic Rankine Cycle Applications, *Industrial & Engineering Chemistry Research* 44 (2005) 5560–5566.
- [13] H. Chen, D. Y. Goswami, E. K. Stefanakos, A review of thermodynamic cycles and working fluids for the conversion of low-grade heat, *Renewable and Sustainable Energy Reviews* 14 (2010) 3059–3067.
- [14] F. Vélez, J. J. Segovia, M. C. Martín, G. Antolín, F. Chejne, A. Quijano, Comparative study of working fluids for a Rankine cycle operating at low temperature, *Fuel Processing Technology*, Available online 22 October 2011, 10.1016/j.fuproc.2011.09.017.
- [15] J. Sun, W. Li, Operation optimization of an organic rankine cycle (ORC) heat recovery power plant, *Applied Thermal Engineering* 31 (2011) 2032–2041.
- [16] Y. Dai, J. Wang, L. Gao, Parametric optimization and comparative study of organic Rankine cycle (ORC) for low grade waste heat recovery, *Energy Conversion and Management* 50 (2009) 576–582.
- [17] G. Taljan, G. Verbic, M. Pantos, M. Sakulin, L. Fickert, Optimal sizing of biomass-fired Organic Rankine Cycle CHP system with heat storage, *Renewable Energy*, Available online 22 October 2011, 10.1016/j.renene.2011.09.034.
- [18] S. Quoilin, R. Aumann, A. Grill, A. Schuster, V. Lemort, H. Spliethoff, Dynamic modeling and optimal control strategy of waste heat recovery Organic Rankine Cycles, *Applied Energy* 88 (2011) 2183–2190.
- [19] S. Quoilin, S. Declaye, B. F. Tchanche, V. Lemort, Thermo-economic optimization of waste heat recovery Organic Rankine Cycles, *Applied Thermal Engineering* 31 (2011) 2885–2893.
- [20] A. Schuster, S. Karellas, E. Kakaras, H. Spliethoff, Energetic and economic investigation of Organic Rankine Cycle applications, *Applied Thermal Engineering* 29 (2009) 1809–1817.

- [21] P. Colonna and T. P. van der Stelt, FluidProp: a program for the estimation of thermophysical properties of fluids, Energy Technology Section, Delft University of Technology, The Netherlands (www.fluidprop.com) (2004).
- [22] Cycle-Tempo, www.cycle-tempo.nl.